Welcome to STN International! Enter x:x

LOGINID: SSSPTA1743BXS

PASSWORD:

TERMINAL (ENTER 1, 2, 3, OR ?):2

```
Welcome to STN International
                 Web Page for STN Seminar Schedule - N. America
NEWS
      1
                 WPIDS/WPIX enhanced with new FRAGHITSTR display format
NEWS
         MAR 15
      2
NEWS
     3
         MAR 16 CASREACT coverage extended
NEWS 4
         MAR 20 MARPAT now updated daily
         MAR 22 LWPI reloaded
NEWS 5
         MAR 30 RDISCLOSURE reloaded with enhancements
NEWS 6
         APR 02 JICST-EPLUS removed from database clusters and STN
NEWS
     7
         APR 30 GENBANK reloaded and enhanced with Genome Project ID field
NEWS 8
         APR 30
                 CHEMCATS enhanced with 1.2 million new records
NEWS 9
NEWS 10 APR 30
                 CA/CAplus enhanced with 1870-1889 U.S. patent records
                 INPADOC replaced by INPADOCDB on STN
NEWS 11
         APR 30
NEWS 12
         MAY 01
                 New CAS web site launched
NEWS 13
         MAY 08
                 CA/CAplus Indian patent publication number format defined
         MAY 14
NEWS 14
                 RDISCLOSURE on STN Easy enhanced with new search and display
                 fields
         MAY 21
                 BIOSIS reloaded and enhanced with archival data
NEWS 15
NEWS 16
         MAY 21
                 TOXCENTER enhanced with BIOSIS reload
NEWS 17
         MAY 21
                 CA/CAplus enhanced with additional kind codes for German
                 patents
NEWS 18
         MAY 22
                 CA/CAplus enhanced with IPC reclassification in Japanese
                 patents
NEWS 19
         JUN 27
                 CA/CAplus enhanced with pre-1967 CAS Registry Numbers
NEWS 20 JUN 29
                 STN Viewer now available
NEWS 21
        JUN 29
                 STN Express, Version 8.2, now available
NEWS 22
         JUL 02
                 LEMBASE coverage updated
NEWS 23 JUL 02
                 LMEDLINE coverage updated
NEWS 24
         JUL 02
                 SCISEARCH enhanced with complete author names
         JUL 02
                 CHEMCATS accession numbers revised
NEWS 25
NEWS 26 JUL 02 CA/CAplus enhanced with utility model patents from China
              29 JUNE 2007: CURRENT WINDOWS VERSION IS V8.2,
NEWS EXPRESS
              CURRENT MACINTOSH VERSION IS V6.0c(ENG) AND V6.0Jc(JP),
              AND CURRENT DISCOVER FILE IS DATED 05 JULY 2007.
NEWS HOURS
              STN Operating Hours Plus Help Desk Availability
NEWS LOGIN
              Welcome Banner and News Items
              For general information regarding STN implementation of IPC 8
NEWS · IPC8
Enter NEWS followed by the item number or name to see news on that
```

specific topic.

All use of STN is subject to the provisions of the STN Customer agreement. Please note that this agreement limits use to scientific research. Use for software development or design or implementation of commercial gateways or other similar uses is prohibited and may result in loss of user privileges and other penalties.

Columbus

FILE 'HOME' ENTERED AT 15:32:57 ON 12 JUL 2007

=> file caplus compendex inspec

COST IN U.S. DOLLARS SINCE FILE TOTAL ENTRY SESSION

FULL ESTIMATED COST . 0.21 0.21

FILE 'CAPLUS' ENTERED AT 15:33:11 ON 12 JUL 2007

USE IS SUBJECT TO THE TERMS OF YOUR STN CUSTOMER AGREEMENT.

PLEASE SEE "HELP USAGETERMS" FOR DETAILS.

COPYRIGHT (C) 2007 AMERICAN CHEMICAL SOCIETY (ACS)

FILE 'COMPENDEX' ENTERED AT 15:33:11 ON 12 JUL 2007

Compendex Compilation and Indexing (C) 2007

Elsevier Engineering Information Inc (EEI). All rights reserved.

Compendex (R) is a registered Trademark of Elsevier Engineering Information Inc.

FILE 'INSPEC' ENTERED AT 15:33:11 ON 12 JUL 2007

Compiled and produced by the IET in association WITH FIZ KARLSRUHE COPYRIGHT 2007 (c) THE INSTITUTION OF ENGINEERING AND TECHNOLOGY (IET)

=> s acrylonitrile

103011 ACRYLONITRILE

=> s 11 and ammoxidation (8w) reactor

63 L1 AND AMMOXIDATION (8W) REACTOR

=> s 12 and fourier (6w) transform (6w) infrared (8w) (spectrometer or spectrophotometer)

1 L2 AND FOURIER (6W) TRANSFORM (6W) INFRARED (8W) (SPECTROMETER L3OR SPECTROPHOTOMETER)

=> display 13 1 ibib abs

L3 ANSWER 1 OF 1 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

2000:725841 CAPLUS

DOCUMENT NUMBER:

133:270789

TITLE:

Apparatus and process for monitor and control of an

ammoxidation reactor with a Fourier transform infrared

spectrometer

INVENTOR(S):

Casal, Hector L.; Azker, Nazaneen; Seely, Michael J.;

Nero, Linda L.; Baldwin, Jean A.

PATENT ASSIGNEE(S):

SOURCE:

Bp Amoco Corp., USA

PCT Int. Appl., 65 pp.

CODEN: PIXXD2

DOCUMENT TYPE:

Patent

LANGUAGE:

English

FAMILY ACC. NUM. COUNT:

PATENT NO.				KIND DATE			APPLICATION NO.						DATE				
				•		-											
WO	2000	0603	36		A1 20001012			1	WO 2	000-1	US84:	14 -		20000329			
	W:	ΑE,	AG,	AL,	AM,	ΑT,	AU,	ΑZ,	BA,	BB,	BG,	BR,	BY,	CA,	CH,	CN,	CR,
		CU,	CZ,	DE,	DK,	DM,	DZ,	EE,	ES,	FI,	GB,	GD,	GE,	GH,	GM,	HR,	HU,
		ID,	IL,	IN,	ΙŞ,	JP,	KE,	KG,	ΚP,	KR,	KZ,	LC,	LK,	LR,	LS,	LT,	LU,
		LV,	MA,	MD,	MG,	MK,	MN,	MW,	MX,	NO,	NZ,	PL,	PT,	RO,	RU,	SD,	SE,
		SG,	SI,	SK,	SL,	ТJ,	TM,	TR,	TT,	TZ,	UA,	UG,	UZ,	VN,	YU,	ZA,	ZW,

AM, AZ, BY, KG, KZ, MD, RU, TJ, TM RW: GH, GM, KE, LS, MW, SD, SL, SZ, TZ, UG, ZW, AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE, BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG DE 10084432 TΟ 20020321 DE 2000-10084432 20000329 TW 475059 В 20020201 TW 2000-89106074 20000412 US 2002055175 **A1** 20020509 US 2001-945464 20010830 В2 US 6607447 20030819 US 2004023407 A1 20040205 US 2003-624022 20030721 PRIORITY APPLN. INFO.: US 1999-282934 A 19990401 WO 2000-US8414 W 20000329 US 2001-945464 A3 20010830 AB The present invention is a method and an apparatus for identifying and quantifying components in an effluent stream from an ammoxidn. reactor. The apparatus comprises a microprocessor and a Fourier Transform IR spectrometer, wherein the microprocessor is programmed to identify and quantify each of the plurality of components based upon the absorbance data and calibration data, the calibration data being obtained from recovery run analyses and calibration analyses in the sample cell. The Fourier

Transform IR spectrometer has a sample cell. The Fourier

Transform IR spectrometer has a sample cell

through which may flow a portion of the effluent stream, an IR source to
emit IR radiation and pass the IR radiation through the effluent stream,
an IR detector to detect transmitted IR radiation at the selected IR
wavelengths and to generate absorbance data due to absorbance of the IR
radiation by the components, wherein each of the components absorbs IR
radiation at one or more of the IR wavelengths, and an output apparatus to
provide the absorbance data to the microprocessor. The apparatus is used in
this case to analyze acrylonitrile reactor effluents. The

method may be applied to utilize the apparatus to provide real-time control of the operation of an ammoxidn. reactor, based on the

anal. results obtained by the FT-IR spectrometer and the calibration model developed therefor.

REFERENCE COUNT:

THERE ARE 4 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

=> FIL STNGUIDE COST IN U.S. DOLLARS SINCE FILE TOTAL ENTRY SESSION FULL ESTIMATED COST 23.89 24.10 DISCOUNT AMOUNTS (FOR QUALIFYING ACCOUNTS) SINCE FILE TOTAL ENTRY SESSION CA SUBSCRIBER PRICE. -0.78-0.78

FILE 'STNGUIDE' ENTERED AT 15:35:48 ON 12 JUL 2007 USE IS SUBJECT TO THE TERMS OF YOUR CUSTOMER AGREEMENT COPYRIGHT (C) 2007 AMERICAN CHEMICAL SOCIETY (ACS)

FILE CONTAINS CURRENT INFORMATION.
LAST RELOADED: Jul 6, 2007 (20070706/UP).

=> s ammoxidation (8w) reactor

- 0 AMMOXIDATION
- 0 REACTOR
- 1. REACTORS
- 1 REACTOR

(REACTOR OR REACTORS)

L4 0 AMMOXIDATION (8W) REACTOR

=> file caplus compendex inspec

COST IN U.S. DOLLARS

SINCE FILE TOTAL
ENTRY SESSION

FULL ESTIMATED COST

DISCOUNT AMOUNTS (FOR QUALIFYING ACCOUNTS)

CA SUBSCRIBER PRICE

SINCE FILE TOTAL
ENTRY SESSION

-0.78

FILE 'CAPLUS' ENTERED AT 15:37:08 ON 12 JUL 2007 USE IS SUBJECT TO THE TERMS OF YOUR STN CUSTOMER AGREEMENT. PLEASE SEE "HELP USAGETERMS" FOR DETAILS. COPYRIGHT (C) 2007 AMERICAN CHEMICAL SOCIETY (ACS)

FILE 'COMPENDEX' ENTERED AT 15:37:08 ON 12 JUL 2007
Compendex Compilation and Indexing (C) 2007
Elsevier Engineering Information Inc (EEI). All rights reserved.
Compendex (R) is a registered Trademark of Elsevier Engineering Information Inc.

FILE 'INSPEC' ENTERED AT 15:37:08 ON 12 JUL 2007 Compiled and produced by the IET in association WITH FIZ KARLSRUHE COPYRIGHT 2007 (c) THE INSTITUTION OF ENGINEERING AND TECHNOLOGY (IET)

=> s ammoxidation (8w) reactor L5 109 AMMOXIDATION (8W) REACTOR

=> s 15 and fourier (6w) transform (6w) infrared (8w) (spectrometer or spectrophotometer) \cdot

1 L5 AND FOURIER (6W) TRANSFORM (6W) INFRARED (8W) (SPECTROMETER OR SPECTROPHOTOMETER)

=> s 15 and acrylonitrile L7 63 L5 AND ACRYLONITRILE

=> s 17 and FTIR L9 0 L7 AND FTIR

=> duplicate remove 17 1-63
'1-63' IS NOT VALID. VALID FILE NAMES ARE 'CAPLUS, COMPENDEX'
You have entered a file name of duplicates to keep that is not referenced by any of the L#s specified for this DUPLICATE command. The file names of duplicates that can be kept are listed above. Please enter one of these file names.
ENTER FILE NAMES OF DUPLICATES TO KEEP:caplus PROCESSING COMPLETED FOR L7
L10 61 DUPLICATE REMOVE L7 CAPLUS (2 DUPLICATES REMOVED)

=> display 110 1-61 ibib abs

L10 ANSWER 1 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 2005:1239957 CAPLUS

DOCUMENT NUMBER: 144:6511

TITLE: Ammoxidation of organic compounds using mixed oxide

catalysts containing molybdenum, bismuth, and iron and

molybdenum-containing activators

INVENTOR(S): Watanabe, Hirokazu; Watanabe, Seigo; Miyaki, Kenichi;

Yamaguchi, Masanori

PATENT ASSIGNEE(S): Dia-Nitrix Co., Ltd., Japan SOURCE: Jpn. Kokai Tokkyo Koho, 11 pp.

CODEN: JKXXAF

DOCUMENT TYPE:

Patent Japanese

LANGUAGE: FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

DATE PATENT NO. KIND APPLICATION NO. DATE _____ ---------______ Α JP 2005325068 20051124 JP 2004-145245 20040514 PRIORITY APPLN. INFO.: JP 2004-145245 20040514

CASREACT 144:6511 OTHER SOURCE(S):

Ammoxidn. of organic compds. is performed using mixed oxide catalysts containing

at least Mo, Bi, and Fe having bulk d. 0.85-1.20 and Fe iron and Mo-containing activators having bulk d. 1.3-1.9 in fluidized-bed reactors, wherein a feed gas-increasing step to increase initial velocity of feed gas in the reactor to 1.05-1.40 times that in the steady state for a time between 0.5 min and 5 h is repeated at least once every 200 h. The activators staying in the bottom of the reactor in the steady state are lifted to the mixed oxide catalyst layer when amount of feed gas is increased and effectively contacted with the catalysts to activate them. Thus, a gaseous mixture of air, NH3, steam, and propylene was fed to a fluidized-bed reactor packed with Mol0Bi0.4Fe4.3Ni5Cr0.8CoSb3.5K0.2Ce0.4P0.2B0.2O52.07(SiO2)35 (preparation given) and ammonium paramolybdate at 200 KPa and 430° while intermittently increasing initial velocity of the feed gas from 0.52 m/s (steady state) to 0.62 m/s only for 1.5 h at a predetd. interval (once every 150 h). Yield of acrylonitrile after 1000 h was 81.5%, vs. 81.6% after 5 h.

L10 ANSWER 2 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

2005:632271 CAPLUS

DOCUMENT NUMBER:

143:115908

TITLE:

Manufacture of acrylonitrile using granular

catalysts

INVENTOR(S):

Watanabe, Seigo; Yanagida, Motoo; Miyaki, Kenichi;

Yamaquchi, Masanori

PATENT ASSIGNEE(S):

Dia-Nitrix Co., Ltd., Japan Jpn. Kokai Tokkyo Koho, 17 pp.

CODEN: JKXXAF

DOCUMENT TYPE:

Patent

LANGUAGE:

SOURCE:

Japanese

FAMILY ACC. NUM. COUNT: 1

PATENT INFORMATION:

	PATENT NO.	KIND	DATE	AP:	PLICATION NO.		DATE
	JP 2005194234	Α	20050721	JP	2004-2912	•	20040108
PRIO	RITY APPLN. INFO.:			JP	2004-2912		20040108
AB	Acrylonitrile is ma	nufactu	red by react	ion	of propylene w	ith mo	01.0
	and NH3 in a fluidi	zed-bed	reactor fil	led	with granular	cataly	sts showi

ing specific particle size distribution while discharging 0.05-1% of the catalysts of 20-44 µm particle size per a day and supplying granular catalysts of specific particle size distribution at 0.03-1% (based on total catalyst) per a day during the reaction. Thus, ammoxidn. of propylene was carried out using Mo12Bi0.5Fe2Ce0.5Cr0.4Ni4Mg1.5Co1K0.07Rb0. 060x(SiO2) while partially replacing the catalyst for 42 days to result in initial and final yield 82.6 and 82.3%, resp.

L10 ANSWER 3 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

2005:634973 CAPLUS

DOCUMENT NUMBER:

143:133797

TITLE:

Method for preparation of acrylonitrile by ammoxidation of propylene using fluidized-bed reactors

INVENTOR(S):
PATENT ASSIGNEE(S):

Tanaka, Isao; Kameo, Hiroshi Dia-Nitrix Co., Ltd., Japan Jpn. Kokai Tokkyo Koho, 8 pp.

CODEN: JKXXAF

DOCUMENT TYPE:

SOURCE:

LANGUAGE:

Patent Japanese

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
JP 2005193172	Α	20050721	JP 2004-3013	20040108
PRIORITY APPLN. INFO.:			JP 2004-3013	20040108

AB The method comprises removing partial particulate catalysts from the reactors, classifying the catalyst particles to obtain fine catalyst particles (diameter 20-44 $\mu m)$, and feeding the fine catalysts with a small amount of fresh catalysts to the reactors so as to improve the flowability of the catalysts and the yield of the product.

L10 ANSWER 4 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

2003:454266 CAPLUS

DOCUMENT NUMBER:

139:36954

TITLE:

Oxidation process in a fluidized-bed reactor

INVENTOR(S):

Fiorentino, Michele; Newton, David; Salem, George

Frederick; Williams, Bruce Leo

PATENT ASSIGNEE(S):

BP Chemicals Limited, UK PCT Int. Appl., 35 pp.

SOURCE:

CODEN: PIXXD2

DOCUMENT TYPE:

Patent

LANGUAGE:

English

FAMILY ACC. NUM. COUNT:

PAT	PATENT NO.				KIN	D	DATE		APPLICATION NO.						DATE		
	2003									WO 2	002-	GB54	15		2	0021	129
	W:							AZ,		BB	B.C.	BD	BV	B 7	CA	CH	CNI
	** .							DM,									
								JP,									
								MK,									
								SG,					-	-	-	-	
								YU,				10,	111,	III,	ın,	11,	14,
	RW:	GH,	•	•	•	•	•	•	•	•		IIG.	7.M	7.W	ΔM	Δ7.	ВY
								AT,									
								LU,									
								GW,							21,	20,	0.,
US	2003														2	0021	126
	7145														_		
CA	2468	500			A1		2003	0612		CA 2	002-	2468	500		2	0021	129
AU	2002	3491	40		A1		2003	0617		AU 2	002-	3491	40		2	0021	129
BR	2002	0147						0831									
EP	1451	135						0901								0021	
	R:	AT,	BE,	CH,	DE,	DK,	ES.	FR.	GB,	GR,	IT,	LI.	ĽŪ,	NL.	SE.	MC.	PT.
								MK,				-	-		-	,	,
JP	2005							0428				5492				0021	129
CN	1639	102			A		2005	0713									
IN	2004											DN13					
ИО	2004	0028	09	•	Α		2004	0702		NO 2	004-	2809			2	0040	702
US	2006	0307	29		A1		2006	0209		US 2	005-	2391	37		. 2	0050	930 .
	7189						2007										

US 2007088175 A1 20070419 US 2006-541678 20061003 P 20011204 PRIORITY APPLN. INFO.: US 2001-334970P US 2002-303769 A3 20021126 WO 2002-GB5415 W 20021129 US 2005-239137 A1 20050930

A process for reacting in a fluid bed reactor at least one oxidizable reactant (e.g., ethane) with mol. oxygen in the presence of a catalytically active fluidized bed of solid particles is described. In this process, a mol. oxygen-containing gas having an oxygen concentration

than that of air is introduced into the fluidized bed while the fluidized bed is maintained in a turbulent regime. The process is suitable for oxidation, ammoxidn. and esterification (i.e., manufacture of vinyl acetate

acetic acid and ethylene) processes, including the production of maleic anhydride, acrylonitrile, ethylene, acetic acid, and vinyl

7 REFERENCE COUNT: THERE ARE 7 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L10 ANSWER 5 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

2003:166990 CAPLUS

DOCUMENT NUMBER:

138:206859

TITLE:

Increased production of acetonitrile as byproduct in

ammoxidation of propylene to acrylonitrile

INVENTOR(S):

Midorikawa, Hideo

PATENT ASSIGNEE(S):

Asahi Kasei Corporation, Japan Jpn. Kokai Tokkyo Koho, 11 pp.

CODEN: JKXXAF

DOCUMENT TYPE:

Patent

LANGUAGE:

SOURCE:

Japanese

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE	
DDTO:	JP 2003064042 RITY APPLN. INFO.:	Α	20030305	JP 2001-258918 JP 2001-258918	20010829	
		in man.	.f.at of .			
AB	ammoxidn. of propyle			acrylonitrile (I) by cat sed reactor are	talytic	
	prepared in higher	yield by	y feeding ≥1	selected from EtOH, Et2	20,	
	HCO2Et, AcOH, Ac2O,	EtOAc,	EtOCH2CH2OE	t, ethylene, MeCHO, and	HOCH2CO2Et	
	at a carbon-base rat	tio to p	propylene 0.0	005-0.2 using MoyBipFeqA	AaBbCcDdOe (A	
	= Ni, Co; $B = K$, Rb	, Cs; C	= Mg, Zn; D	= rare earth element;	<i>y</i> =	
				5d; p = 0.01-5.0; q = 0		
	4-10; b = 0.01-2; c	= 0-5;	d = 0-5; e :	is determined by valency	y requirements)	
	supported on silica	while o	controlling (02 concentration in the	outlet gas	
0.1-	1.5					

volume%. Thus, a gas mixture containing propylene, NH3, and air and EtOH were fed

to a reactor packed with Mol1.8Bi0.45Ce0.90Fe1.8Ni5.0Mg2.0K0.09Rb0.05Oe at 430° , 150 kPa, and contact time 5.7 s g/mL to give 82.4% I and 2.5% MeCN after 100 h, vs. 82.5 and 2.0%, resp., for a control reaction using no EtOH.

L10 ANSWER 6 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 2003:166989 CAPLUS

DOCUMENT NUMBER:

138:206858

TITLE:

Increased production of acetonitrile and prussic acid

as byproducts of acetonitrile manufacture

INVENTOR(S): Midorikawa, Hideo

PATENT ASSIGNEE(S):

Asahi Kasei Corporation, Japan

SOURCE: Jpn. Kokai Tokkyo Koho, 11 pp.

CODEN: JKXXAF

DOCUMENT TYPE: LANGUAGE:

Patent Japanese

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PATENT NO. KIND DATE APPLICATION NO. DATE

----JP 2003064041 A 20030305 JP 2001-258920 20010829
PRIORITY APPLN. INFO.: JP 2001-258920 20010829

MeCN and HCN as byproducts in manufacture of acrylonitrile (I) by catalytic ammoxidn. of propylene in a fluidized-bed reactor are prepared in higher yield by feeding ≥1 selected from EtOAc, acetone, and MeOEt at a carbon-base ratio to propylene 0.005-0.2 using MoyBipFeqAaBbCcDdOe (A = Ni, Co; B = K, Rb, Cs; C = Mg, Zn; D = rare earth element; y = 1.02x-1.12x; x = 1.5p + q + a + c + 1.5d; p = 0.01-5.0; q = 0.1-5; a = 4-10; b = 0.01-2; c = 0-5; d = 0-5; e is determined by valency requirements) supported on silica while controlling O2 concentration in the outlet gas 0.1-1.5 volume%. Thus, a gas mixture containing

propylene, NH3, and air and acetone were fed to a reactor packed with Moll.8Bi0.45Ce0.90Fel.8Ni5.0Mg2.0K0.09Rb0.050e at 430°, 150 kPa, and contact time $5.7~\rm s\cdot g/mL$ to give $82.4\%~\rm I$, $3.2\%~\rm MeCN$, and $5.5\%~\rm HCN$ after 100 h, vs. 82.5, 2.0, and 4.0%, resp., for a control reaction using no acetone.

L10 ANSWER 7 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 2003:14357 CAPLUS

DOCUMENT NUMBER: 138:90226

TITLE: Continuous and simultaneous manufacture of unsaturated

nitrile and hydrocyanic acid

INVENTOR(S): Sano, Kazuhiko

PATENT ASSIGNEE(S): Asahi Kasei Corporation, Japan SOURCE: Jpn. Kokai Tokkyo Koho, 7 pp.

CODEN: JKXXAF

DOCUMENT TYPE: Patent LANGUAGE: Japanese

FAMILY ACC. NUM. COUNT: 1

PATENT INFORMATION:

PATENT NO. KIND DATE APPLICATION NO. DATE

JP 2003002870 A 20030108 JP 2001-187699 20010621
PRIORITY APPLN. INFO.: JP 2001-187699 20010621

Title compds. are manufactured in a fluidized-bed reactor by ammoxidn of (A) propylene, isobutylene, and/or tert-butanol and (B) MeOH and/or HCHO with NH3 and O-containing gas in the presence of MoyBipFeqAaBbCcDdOf (A = Ni, Co; B = K, Rb, Ce; C = Mg, Zn; D = rare earth element; d/(p + d) = 0.6-0.8; p + d = 0.5-2.0; q = 0.1-3; a = 4-10; b = 0.01-2; c = 0-3; x = 1.5p + q + a + c + 1.5d; y = 1.02x - 1.10x) while adjusting the O concentration of the exhaust gas to 0.3-1.5 volume%. Thus, a propylene-NH3-air mixture and gaseous MeOH were passed through Mo11.7Bi0.20Ce0.40Fe2.0Ni5.6Mg2.2K0.07Cs0.040x/Si02-packed reactor at O concentration 0.35 volume% for 720 h to give 80.8% acrylonitrile, 6.5% HCN, and 0.8% acrolein, vs. poor yield, when the O concentration was 0.25 volume% instead.

L10 ANSWER 8 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 2003:666022 CAPLUS

DOCUMENT NUMBER: 140:304097

TITLE: Comparison of proposals for the remodeling of the

ammoxidation reactor in an

acrylonitrile apparatus

Chen, Tao AUTHOR(S):

CORPORATE SOURCE:

PetroChemical Plant, Lanzhou Prochemical Co., PetroChina, Lanzhou, 730060, Peop. Rep. China Shihua Jishu Yu Yingyong (2003), 21(4), 273-275

CODEN: SJYIF4; ISSN: 1009-0045

PUBLISHER: Shihua Jishu Yu Yingyong Bianjibu

DOCUMENT TYPE: Journal LANGUAGE: Chinese

An MB 98 catalyst had selectivity for acrylonitrile 82.0% and conversion of propylene 98.5%, compared with 81.4 and 97.6, resp., for an MB 96 catalyst. A remodeling included a cyclone, an air distributing plate, a reactant distributor, and a heat release system.

L10 ANSWER 9 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

2002:927867 CAPLUS ACCESSION NUMBER:

DOCUMENT NUMBER: 138:26375

Two-stage method for gas-solid contact in bubbling TITLE:

fluidized-bed reactors for catalytic and non-catalytic

reactions

Choudhary, Vasant Ramchandra; Choudhary, Tushar Vasant INVENTOR(S):

Council of Scientific & Industrial Research, India PATENT ASSIGNEE(S):

SOURCE: U.S. Pat. Appl. Publ., 10 pp.

CODEN: USXXCO

DOCUMENT TYPE:

SOURCE:

Patent

LANGUAGE:

English

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PAT	ENT NO.	KIND	DATE	APPLICATION NO.	DATE
US	2002179489	A 1	20021205	US 2001-817744	20010326
US	6894183	В2	20050517		
US	2004122116	A1	20040624	US 2003-725723	20031202
US	7022307	B2	20060404		

US 2001-817744 PRIORITY APPLN. INFO.: A3 20010326

A two-stage method for contacting of gases and solids in a bubbling fluidized-bed reactor (for catalytic and noncatalytic reactions) was developed in which the first stage involves fluidization with bubbling, and the second stage involves the formation of the bubbling bed. In the first stage, a primary gas, containing the reactant(s), is introduced into the reactor (with bed length to bed diameter ratio .ltorsim.5.0:1) through a primary gas distributor located at the reactor bottom at a superficial gas velocity, Up, that is close or equivalent to the min. fluidization velocity, Umf, required to obtain an emulsion phase with little or no formation of gas bubbles. In the second stage, gas bubbles in the incipiently fluidized bed (formed in stage 1) are formed by introducing a secondary gas through a secondary gas distributor located immediately above the primary gas distributor. This secondary gas is selected from one of the reactants which is used in excess of that required for reaction stoichiometry (e.g., steam), at a superficial gas velocity, Us. Us is related to the Up (of the primary gas) such that a Us/Up is 0.5-10.0:1, preferably 1-5:1. Typical reactions that can be handled by the bubbling fluidized bed include vapor-phase hydrogenation of nitrobenzene and nitrotoluene isomers to aniline and the corresponding toluidine, methane conversion to synthesis gas, ammoxidn. of propylene to acrylonitrile, propylene oxidation to acrolein, oxidation of acrolein to acrylic acid, regeneration of coked hydrocarbon cracking catalyst, ethane

oxychlorination, Fischer-Tropsch reaction, and heavy oil hydrocracking. REFERENCE COUNT: THERE ARE 1 CITED REFERENCES AVAILABLE FOR THIS 1 RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT L10 ANSWER 10 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

2002:755239 CAPLUS

DOCUMENT NUMBER:

137:263439

TITLE:

Process for recovery of olefinically unsaturated

nitriles

INVENTOR(S):

Ward, Gregory J.; Monical, Valerie S.

PATENT ASSIGNEE(S):

USA

2

SOURCE:

U.S. Pat. Appl. Publ., 6 pp., Cont.-in-part of U.S.

Ser. No. 333,431, abandoned.

CODEN: USXXCO

DOCUMENT TYPE:

Patent

LANGUAGE:

English

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.		DATE
				_	
US 2002143131	A1	20021003	US 2001-964296		20010920
US 6860971	В2	20050301	•		
PRIORITY APPLN. INFO.:		•	US 1998-89352P	P	19980615
			US 1999-333431	B2	19990615

A process is described for the recovery of acrylonitrile from an AΒ ammoxidn. reactor effluent stream containing acrylonitrile, water, and organic impurities. The process includes the steps of (a) quenching an ammoxidn. reactor effluent stream that includes acrylonitrile, water, and organic impurities with an aqueous quench stream, thereby producing a cooled reactor effluent stream; (b) passing the cooled reactor effluent stream through an absorption column, thereby generating an absorber bottoms stream that includes water, acrylonitrile, and organic impurities; and (c) passing the absorber bottoms stream through a single recovery/stripper column, generating an acrylonitrile-rich overhead stream, a lean water side stream, and a recovery/stripper bottoms stream that includes organic impurities. The acrylonitrile-rich overhead stream can be passed through a decanter to sep. water from acrylonitrile. The lean water side stream can be recycled for use in the absorption column.

REFERENCE COUNT:

THERE ARE 2 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L10 ANSWER 11 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

2

ACCESSION NUMBER:

2002:708789 CAPLUS

DOCUMENT NUMBER:

SOURCE:

137:203033

TITLE:

Method for stopping the ammoxidation

INVENTOR(S):

Nakamura, Toshio; Arai, Hachiro; Sawada, Yoshikazu;

Yamagishi, Yoichi

PATENT ASSIGNEE(S):

Daiya Nitrics K. K., Japan Jpn. Kokai Tokkyo Koho, 4 pp.

CODEN: JKXXAF

DOCUMENT TYPE:

Patent

1

LANGUAGE:

Japanese

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
JP 2002265431	Α	20020918	JP 2001-62256	20010306
PRIORITY APPLN. INFO.	:		JP 2001-62256	20010306

In the title method for stopping the ammoxidn, of propylene or AB isobutylene in a fluidized bed reactor, an inert gas (with volume 1 to 1000 times that of the catalyst bed) is supplied to the reactor after the supply of the oxygen-containing gas, ammonia and propylene or isobutylene to the reactor is stopped. Or, after the supply of ammonia and propylene

or isobutylene to the reactor is stopped, the supply of the oxygen-containing gas (with volume 0.5 to 5 times that of the catalyst bed) to the reactor is continued. Or, after the supply of propylene or isobutylene to the reactor is stopped, the supply of the oxygen-containing gas and ammonia to the reactor is continued. The title method ensures the safety of the work and prevents the deterioration of the catalyst.

L10 ANSWER 12 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 2002:626082 CAPLUS

DOCUMENT NUMBER: 137:140912

TITLE: Catalysts pretreatment for production of

acrylonitrile

Nakamura, Toshio; Arai, Hachiro; Sawada, Yoshikazu; INVENTOR(S):

Yamaquchi, Masanori

Daiya Nitrics K. K., Japan PATENT ASSIGNEE(S):

Jpn. Kokai Tokkyo Koho, 4 pp. SOURCE:

CODEN: JKXXAF

Patent DOCUMENT TYPE: LANGUAGE: Japanese

FAMILY ACC. NUM. COUNT: 1

PATENT INFORMATION:

KIND DATE APPLICATION NO. PATENT NO. ____ _____ _____ 20010206 20010206 JP 2002233759 A 20020820 JP 2001-29319 PRIORITY APPLN. INFO.: JP 2001-29319

Production method of acrylonitrile via ammoxidn. of

propylene in fluidized reactor, catalysts are pretreated by

filling the catalysts in the reactor with the oxygen gas concentration 6-30% at 300-450° for 1-100 h.

L10 ANSWER 13 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 2002:171448 CAPLUS

DOCUMENT NUMBER: 136:232678

Process for increasing the yield of hydrocyanic acid TITLE:

in acrylonitrile manufacture

INVENTOR(S): Arai, Hachiro; Sawada, Yoshikazu; Nakamura, Toshio

INVENTOR(S): Arai, Hachiro; Sawada, Yoshikazu; N
PATENT ASSIGNEE(S): Mitsubishi Rayon Co., Ltd., Japan

SOURCE: Jpn. Kokai Tokkyo Koho, 5 pp.

CODEN: JKXXAF

DOCUMENT TYPE: Patent LANGUAGE: Japanese

FAMILY ACC. NUM. COUNT: 1

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE		
JP 2002069048	Α	20020308	JP 2000-258803	20000829		
PRIORITY APPLN. INFO.:			JP 2000-258803	20000829		

In the process for manufacturing acrylonitrile by ammoxidn. AB of propylene or propane using a fluidized layer reactor, methanol and water vapor are introduced at the speed of 5 to 70 m/s into the catalyst layer from the gas inlet located at the upper part of the fluidized layer; the water/methanol mol ratio is 0.5 to 10. The title process gives 115% increase rate in the yield of hydrocyanic acid.

L10 ANSWER 14 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 2002:331896 CAPLUS

136:342644 DOCUMENT NUMBER:

Apparatus and process for heat exchange with fluid TITLE:

INVENTOR(S): Becker, Stanley John; Fiorentino, Michele; Williams, Bruce Leo; Bristow, Timothy Crispin; Newton, David

PATENT ASSIGNEE(S):

BP Chemicals Limited, UK Eur. Pat. Appl., 12 pp.

CODEN: EPXXDW

DOCUMENT TYPE:

SOURCE:

LANGUAGE:

Patent English

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PA!	PATENT NO.		•	KIND DATE		APPLICATION NO.						DATE				
EP	1202017			A2	-	2002	0502	EP	2	001-	3082	 91		. 2	0010	928
EP	1202017			A 3		2004	1215				,					
EP	1202017	•		В1		2006	0517									
	R: AT	, BE,	CH,	DE,	DK,	ES,	FR,	GB, G	R,	IT,	LI,	LU,	NL,	SE,	MC,	PT,
	ΙE	, SI,	LT,	LV,	FI,	RO,	MK,	CY, A	L,	TR						
US	2002074	107		A 1		2002	0,620	US	20	001-	9648	81		. 5	0010	928
US	6602476	•		В2		2003	0805									
AT	326674			Т		2006	0615	AT	20	001-	3082	91		2	0010	928
SG	115413			A1		2005	1028	SG	20	001-	6125			2	0011	003
IN	2001MU0	0980		Α		2005	0819	IN	20	001-	MU98	0		2	0011	800
NO	2001005	219		Α		2002	0429	NO	20	001-	5219			2	0011	025
	2001004			Α		2002	0702	BR	20	001-	4818			2	0011	025
JP	2002213	886		A		2002	0731	JP	20	001-	3284	35		2	0011	025
TW	592833			В		2004	0621	TW	20	001-	9012	6419		2	0011	025
RU	2289075			C2		2006	1210	RU	20	001-	1287	25		2	0011	025
CN	1350881			Α	·	2002	0529	CN	20	001-	1375	15		2	0011	026
ORITY	Y APPLN.	INFO	. :					GB	20	000-	2624	2	7	A 2	0001	026

AB Apparatus and process for heat exchange with fluid beds comprises heat-exchange tubes located longitudinally with respect to the axis of a fluidization zone with a rectangular pitch, one side of which having a length (x) at least one and a half times the length (y) of the other side and/or with a triangular pitch, having two sides each at least one and a half times the length of the shortest side reduces the impact of the heat-exchange tubes on the fluidization characteristics of the fluid bed. The invention is particularly suitable for oxidation reactions using mol. oxygen-containing gas in

the presence of a fluid bed of fluidizable catalyst, such as (a) the acetoxylation of olefins, (b) the oxidation of ethylene to acetic acid and/or the oxidation of ethane to ethylene and/or acetic acid, (c) the ammoxidn. of propylene and/or propane to acrylonitrile and (d) the oxidation of C4's to maleic anhydride.

L10 ANSWER 15 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

2001:50547 CAPLUS

DOCUMENT NUMBER:

134:117616

.TITLE:

Sparger for oxygen injection into fluidized-bed

reactor

INVENTOR(S):

Trott, Louis Rocco; Gustaferro, Robert Angelo; Hepfer,

Robert Paul; Miller, Craig Timothy; Carlsson,

Stig-Axel; Close, Benjamin Wayne

PATENT ASSIGNEE(S):

Standard Oil Company, USA

SOURCE:

PCT Int. Appl., 23 pp.

CODEN: PIXXD2

DOCUMENT TYPE:

Patenț

LANGUAGE:

English

FAMILY ACC. NUM. COUNT: 1

PATENT NO:	KIND	DATE	APPLICATION NO.	DATE
WO 2001003823	A1	20010118	WO 2000-US14981	20000531

```
AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CR,
             CU, CZ, DE, DK, DM, DZ, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU,
             ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU,
             LV, MA, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE,
             SG, SI, SK, SL, TJ, TM, TR, TT, TZ, UA, UG, UZ, VN, YU, ZA, ZW
         RW: GH, GM, KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZW, AT, BE, CH, CY,
             DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE, BF, BJ,
             CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG
                                20020319
                                            US 1999-352465
    US 6358483
                        B1
                                                                     19990713
                                             CA 2000-2379141
     CA 2379141
                          A1
                                20010118
                                                                     20000531
     BR 2000012412
                          Α
                                20020402
                                             BR 2000-12412
                                                                     20000531
                                20020410
                                             EP 2000-937988
     EP 1194224
                          Α1
                                                                     20000531
    EP 1194224
                          В1
                                20041215
             AT, BE, CH, DE, DK, ES, FR, GB, GR, IT, LI, LU, NL, SE, MC, PT,
             IE, SI, LT, LV, FI, RO
    TR 200200030
                                20021121
                                             TR 2002-30
                          Т2
                                                                     20000531
                          \mathbf{T}
                                             JP 2001-509288
     JP 2003504180
                                20030204
                                                                     20000531
     RU 2238139
                          C2
                                20041020
                                             RU 2002-102863
                                                                     20000531
    AT 284752
                          Т
                                20050115
                                            AT 2000-937988
                                                                     20000531
                          Т3
    ES 2232458
                                20050601
                                             ES 2000-937988
                                                                     20000531
                          В1
                                20070330
                                             RO 2002-28
    RO 121321
                                                                     20000531
                          В
                                             TW 2001-90100786
                                20030411
    TW 527219
                                                                     20010112
                          Α
                                20030409
                                             ZA 2002-192
    ZA 2002000192
                                                                     20020109
                          Α
                                20020930
                                             BG 2002-106300
    BG 106300
                                                                     20020114
     BG 64438
                          В1
                                20050228
     IN 2002MN00048
                          Α
                                20060915
                                             IN 2002-MN48
                                                                     20020115
                                             US 1999-352465
PRIORITY APPLN. INFO.:
                                                                 A 19990713
                                             WO 2000-US14981
                                                                 W 20000531
    A sparger includes a conduit for conducting an oxygen feed, a nozzle
     to the outside of the sparger, the nozzle including an orifice and a
    shroud, and insulation surrounding the conduit and also the shroud
     substantially the full length of the shroud. A method is provided for
    producing acrylonitrile via propane ammoxidn., comprising
```

connected to the conduit for passage of the oxygen feed from the conduit introducing propane and ammonia feeds into a fluidized-bed reactor, and introducing an oxygen feed into the fluid bed through at least one insulated and jacketed sparger nozzle for reacting with at least one of the propane feed and ammonia feed in the presence of a fluid bed catalyst. REFERENCE COUNT: THERE ARE 5 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L10 ANSWER 16 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

2001:718962 CAPLUS

DOCUMENT NUMBER:

135:274550

TITLE:

Operation of heads column for the recovery of acrylonitrile, methacrylonitrile or hydrogen

cyanide

INVENTOR(S):

Godbole, Sanjay P.

PATENT ASSIGNEE(S):

The Standard Oil Company, USA

SOURCE:

U.S., 6 pp. CODEN: USXXAM

DOCUMENT TYPE:

Patent

LANGUAGE:

English

FAMILY ACC. NUM. COUNT:

PAT	PATENT NO.				KIND DATE				APPL	ICAT	DATE						
	6296 2003		 41		B1 A1		2001 2003			US 1 WO 2					_	9990 0010	
"0		AE,	AG,	•	AM,	AT,	AU,	AZ,	BA,	BB,	BG,	BR,	BY,	•	CA,	CH,	CN,
		co,	CR,	CU,	CZ,	DE,	DK,	DM,	DZ,	EC,	EE,	ES,	FΙ,	GB,	GD,	GE,	GH,

```
GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR,
            LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, MZ, NO, NZ, PL, PT,
            RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, TZ, UA, UG, UZ,
            VN, YU, ZA, ZW
        RW: GH, GM, KE, LS, MW, MZ, SD, SL, SZ, TZ, UG, ZW, AT, BE, CH, CY,
            DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE, TR, BF,
            BJ, CF, CG, CI, CM, GA, GN, GQ, GW, ML, MR, NE, SN, TD, TG
                               20030310
                                          AU 2001-285149
    AU 2001285149
                         Α1
                                                                   20010821
    EP 1419140
                         .A1
                                20040519
                                           EP 2001-964272
                                                                   20010821
            AT, BE, CH, DE, DK, ES, FR, GB, GR, IT, LI, LU, NL, SE, MC, PT,
            IE, SI, LT, LV, FI, RO, MK, CY, AL, TR
                               20040817
                                           BR 2001-17105
    BR 2001017105
                         Α
                                                                   20010821
    CN 1545499
                         Α
                                20041110
                                           CN 2001-823567
                                                                   20010821
                         Т
                                            JP 2003-523205
    JP 2005501119
                               20050113
                                                                   20010821
                         C1
                                           RU 2004-107845
    RU 2263108
                               20051027
                                                                   20010821
    US 2002029952
                         A1
                               20020314
                                           US 2001-945228
                                                                   20010831
                               20040921
    US 6793776
                         В2
                         Α
    ZA .2004001115
                               20041118
                                           ZA 2004-1115
                                                                  20040211
                        Α
                               20060310
                                           IN 2004-DN346
    IN 2004DN00346
                                                                   20040216
    MX 2004PA01556
                         Α
                               20040517
                                           MX 2004-PA1556
                                                                   20040219
PRIORITY APPLN. INFO.:
                                           US 1999-227665
                                                               A 19990108
                                           WO 2001-US26104
                                                               W 20010821
    A process for the recovery of acrylonitrile, methacrylonitrile
    or hydrogen cyanide obtained from the reactor effluent of an ammoxidn.
    reaction of propane, propylene or isobutylene comprises passing the
```

or hydrogen cyanide obtained from the reactor effluent of an ammoxidn. reaction of propane, propylene or isobutylene comprises passing the reactor effluent through an absorber column, a recovery column and a heads column comprising a feed tray wherein the improvement comprises operating the heads column in a manner which inhibits the formation of an aqueous phase above the feed tray of the heads column; wherein the operating manner of the heads column comprises feeding more hydrogen cyanide to the heads column to achieve conditions equivalent to higher reflux ratio and wherein the feeding is selected from the group consisting of (a) recycling purified HCN to the heads column and (b) operating the ammoxidn. reactor, in a manner to produce the reactor effluent with high concentration of HCN.

REFERENCE COUNT:

THERE ARE 9 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L10 ANSWER 17 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

9

ACCESSION NUMBER:

2001:918856 CAPLUS

DOCUMENT NUMBER:

136:39565

TITLE:

Three-phase fluidized-bed reactors with separate

inlets for injection of liquids and gases

INVENTOR(S):

Bristow, Timothy Crispin; Clarke, Robert William;

Williams, Bruce Leo; Reid, Ian Allan Beattie; Newton,

David; Fiorentino, Michele; Becker, Stanley John

PATENT ASSIGNEE(S):

BP Chemicals Limited, UK

SOURCE:

Eur. Pat. Appl., 8 pp.

CODEN: EPXXDW

DOCUMENT TYPE:

Patent

LANGUAGE:
FAMILY ACC. NUM. COUNT:

English

PAT	ENT	NO.			KIN	D	DATE		· I	APPL	ICAT	ION	NO.		D	ATE	•
						-			-						_		
EP	1163	954		•	A2		2001	1219 [°]	F	EP 2	001-	3044	80		2	0010	522
ΕP	1163	954			A3		2004	0114		•							
	R:	AT,	BE,	CH,	DE,	DK,	ES,	FR,	GB,	GR,	IT,	LI,	LU,	NL,	SE,	MC,	PT,
-		IE,	SI,	LT,	LV,	FI,	RO										
SG	1019	77			A 1		2004	0227	5	SG 2	001-	3331			2	0010	604
IN	2001	MU00	529		Α		2005	0812]	[N 2	001-	MU52	9		2	0010	606

US 2002016374	A1	20020207	US	2001-877227		20010611
US 6913734	В2	20050705				
NO 2001002909	Α	20011217	NO	2001-2909		20010613
JP 2002053498	Α	20020219	JP	2001-179397	•	20010613
BR 2001002385	Α	20020430	BR	2001-2385		20010613
TW 233838	В	20050611	TW	2001-90114262		20010613
RU 2257374	C2	20050727	RU	2001-115767		20010613
CN 1328871	Α	20020102	CN	2001-121016		20010614
us 2005209101	A1	20050922	US	2005-124141		20050509
PRIORITY APPLN. INFO.:			GB	2000-14584	Α	20000614
			US	2001-877227	A3	20010611

A fluidized-bed reactor for heterogeneous gas-phase reactions involves contacting a gaseous reactant with at least one liquid (e.g., a second reactant or a coolant) in the presence of a solid catalyst fluidized bed, in which the injection of gas(es) is carried out through a sep. inlet from that for ligs. The apparatus can be used for oxidation reactions, such as oxidation

of ethane to ethylene or acetic acid, oxidation of ethylene to acetic acid, acetoxylation of ethylene to vinyl acetate, ammoxidn. of propylene or propane to acrylonitrile, and the oxidation of C4-hydrocarbons to maleic anhydride.

L10 ANSWER 18 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 2001:918855 CAPLUS

DOCUMENT NUMBER:

136:39564

TITLE: Inert gas for introduction of oxygen-containing feed gas into fluidized-bed oxidation reactors and process

for oxidation reactions

INVENTOR(S): Bristow, Timothy Crispin; Clarke, Robert William;

Williams, Bruce Leo; Colman, Derek Alan; Reid, Ian

Allan Beattie; Newton, David; Becker, Stanley John

BP Chemicals Limited, UK PATENT ASSIGNEE(S):

SOURCE: Eur. Pat. Appl., 8 pp.

CODEN: EPXXDW

DOCUMENT TYPE: Patent LANGUAGE: English

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

	PAT	ENT	NO.			KINI)	DATE	•	AP	PL	ICAT	ION 1	NO.		D	ATE	
	EP	1163	 953			A2	•	2001	1219	EP	2	001-	3044	 85		2	0010	522
	ΕP	1163	953			A3		2004	0114									
		R:	ΑT,	BE,	CH,	DE,	DK,	ES,	FR,	GB, G	R,	IT,	LI,	LU,	NL,	SE,	MC,	PT,
			IE,	SI,	LT,	LV,	FI,	RO										
	CA	2349	807			A1		2001	1214	C.A	. 2	001-	2349	807		2	0010	530
	SG	1007	17			A 1		2003	1226	SG	2	001-	3329			2	0010	604
	US	2002	0063	68		A1		2002	0117	US	2	001-	8772	49		2	0010	611
	JP	2002	0589	89		Α		2002	0226	JP	. 2	001-	1793	96		2	0010	613
	BR	2001	0023	84		Α		2002	0423	BR	2	001-	2384			2	0010	613
	TW	5412	06			В		2003	0711	TW	2	001-	9011	4268		2	0010	613
	CN	1328	989			Α		2002	0102	CN	2	001-	1210	17		2	0010	614
PRIOF	RITY	APP	LN.	INFO	. :					GB	2	000-	14580	C	7	A 2	0000	614
	_						_											

A reactor, especially for fluidized-bed heterogeneous oxidation reactions, is AΒ equipped with an inlet pipe, for introduction of a mol. oxygen-containing gas reactant, that is surrounded by an inert fluid (i.e., an inert gas). This inlet pipe also has a means for suppressing any entry of reactor contents (e.g., flame, reagents, catalysts, products, etc.) into the inlet pipe that would react with the mol. oxygen-containing reactant prior to entrance into the reactor. The apparatus can be used for oxidation reactions, such as oxidation of ethane to ethylene or acetic acid, oxidation of ethylene to acetic acid, acetoxylation of ethylene to vinyl acetate, ammoxidn. of propylene

or propane to acrylonitrile, and the oxidation of C4-hydrocarbons to maleic anhydride.

L10 ANSWER 19 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 2001:128803 CAPLUS

DOCUMENT NUMBER: 134:224572

TITLE: A pilot plant study and 2-D dispersion-reactor model

for a high-density riser reactor

AUTHOR(S): Wei, F.; Wan, X.; Hu, Y.; Wang, Z.; Yang, Y.; Jin, Y.

Department of Chemical Engineering, Tsinghua CORPORATE SOURCE:

University, Beijing, 100084, Peop. Rep. China

Chemical Engineering Science (2001), 56(2), 613-620 SOURCE:

CODEN: CESCAC; ISSN: 0009-2509

Elsevier Science Ltd. PUBLISHER:

DOCUMENT TYPE: Journal LANGUAGE: English

The radial concentration profiles of reactant concns. in a pilot plant high-d.

riser propylene ammoxidn. reactor were sampled and analyzed and the extreme maldistribution of the profiles were found.

two-dimensional dispersion-reactor model was proposed to simulate the selective oxidization that taken place in the riser, which considered the influences of axial and lateral gas mixing, the non-uniformity of radial solids concentration and gas-velocity profiles on the reactor. The model can successfully predict the axial and radial profiles of concns. sampled in the pilot plant. Simulation results indicate that the non-uniformity in radial catalyst concentration and gas-velocity distribution as well as insufficient lateral gas mixing result in a significant loss of selectivity and yield of acrylonitrile. The scale-up effect and the interdependence of the reaction rate, the non-uniformity of catalyst

concentration and the requirement of gas mixing are discussed.

THERE ARE 21 CITED REFERENCES AVAILABLE FOR THIS 21 REFERENCE COUNT: RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L10 ANSWER 20 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

2000:725841 CAPLUS ACCESSION NUMBER:

133:270789 DOCUMENT NUMBER:

TITLE: Apparatus and process for monitor and control of an

> ammoxidation reactor with a Fourier transform infrared spectrometer

Casal, Hector L.; Azker, Nazaneen; Seely, Michael J.; INVENTOR(S):

Nero, Linda L.; Baldwin, Jean A.

PATENT ASSIGNEE(S): Bp Amoco Corp., USA

SOURCE: PCT Int. Appl., 65 pp.

CODEN: PIXXD2

DOCUMENT TYPE:

Patent LANGUAGE: English

FAMILY ACC. NUM. COUNT:

PA:	PATENT NO.		•		KIN	D :	DATE			APPL	ICAT	ION 1	NO.		D.	ATE	
						_						·					
WO	2000	0603	36		A1		2000	1012	1	WO 2	000-	US84	14		2	0000	329
	W:	ΑE,	AG,	AL,	AM,	AT,	ΑU,	AZ,	BA,	BB,	BG,	BR,	BY,	CA,	CH,	CN,	CR,
		CU,	CZ,	DE,	DK,	DM,	DZ,	EE,	ES,	FI,	GB,	GD,	GE,	GH,	GM,	HR,	HU,
		ID,	IL,	IN,	IS,	·JP,	ΚE,	KG,	KP,	KR,	ΚZ,	LC,	LK,	LR,	LS,	LT,	LU,
		LV,	MA,	MD,	MG,	MK,	MN,	MW,	MX,	NO,	ΝZ,	PL,	PT,	RO,	RU,	SD,	SE,
		SG,	SI,	SK,	SL,	TJ,	TM,	TR,	TT,	TZ,	UA,	UG,	UZ,	VN,	YU,	ZA,	ZW,
		AM,	ΑŻ,	BY,	KG,	KZ,	MD,	RU,	ТJ,	TM							
	RW:	GH,	GM,	KE,	LS,	MW,	SD,	SL,	SZ,	TZ,	UG,	ZW,	AT,	BE,	CH,	CY,	DE,
		DK,	ES,	FI,	FR,	GB,	GR,	ΙE,	IT,	LU,	MC,	NL,	PT,	SE,	BF,	ВJ,	CF,
		CG,	CI,	CM,	GΑ,	GN,	GW,	ML,	MR,	ΝE,	SN,	TD,	TG				
DE	1008	4432			TO		2002	0321		DE 2	-000	1008	4432		2	0000	329

TW 475059	В	20020201	TW	2000-89106074		20000412
US 2002055175	A1	20020509	US	2001-945464		20010830
US 6607447	B2	20030819				
US 2004023407	A1	20040205	US	2003-624022		20030721
PRIORITY APPLN. INFO.:			US	1999-282934	Α	19990401
		•	WO	2000-US8414	W	20000329
			US	2001-945464	A 3	20010830

AB The present invention is a method and an apparatus for identifying and quantifying components in an effluent stream from an ammoxidn. reactor. The apparatus comprises a microprocessor and a Fourier Transform IR spectrometer, wherein the microprocessor is programmed to identify and quantify each of the plurality of components based upon the absorbance data and calibration data, the calibration data being obtained from recovery run analyses and calibration analyses in the sample cell. The Fourier Transform IR spectrometer has a sample cell through which may flow a portion of the effluent stream, an IR source to emit IR radiation and pass the IR radiation through the effluent stream, an IR detector to detect transmitted IR radiation at the selected IR wavelengths and to generate absorbance data due to absorbance of the IR radiation by the components, wherein each of the components absorbs IR radiation at one or more of the IR wavelengths, and an output apparatus to provide the absorbance data to the microprocessor. The apparatus is used in this case to analyze acrylonitrile reactor effluents. The method may be applied to utilize the apparatus to provide real-time control of the operation of an ammoxidn. reactor, based on the anal. results obtained

by the FT-IR spectrometer and the calibration model developed therefor. REFERENCE COUNT: THERE ARE 4 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L10 ANSWER 21 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

2000:784407 CAPLUS

DOCUMENT NUMBER:

133:335634

TTTLE:

SOURCE:

Hybrid ammoxidation reactor and

ammoxidation process for propylene conversion into

acrylonitrile

INVENTOR(S):

Zhou, Lubo; Dennler, W. Patrick; Oroskar, Anil R.; Vora, Bipin V.; Abrevaya, Hayim; Stine, Laurence O.

PATENT ASSIGNEE(S):

UOP LLC, USA U.S., 15 pp. CODEN: USXXAM

Patent

DOCUMENT TYPE: LANGUAGE:

English

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
	•			
US 6143915	Α	20001107	US 1998-198300	19981123
US 6649130	B1	20031118	US 2000-635953	20000810
PRIORITY APPLN. INFO.:			US 1998-198300	A3 19981123

A hybrid reactor arrangement provides a reactive design that achieves AB higher acrylonitrile yield and lower catalyst circulating rate. The hybrid reactor design first passes a mixture of reactants and catalyst through a circulating bubbling bed reaction section. Heat-exchange coils or other cooling medium in the bubbling bed reactor section maintain temperature

in a range that will maximize the selectivity of reactants to the acrylonitrile product. The bubbling bed reactor section provides the initial conversion of the reactant. A circulating fluidized bed reaction zone finishes the conversion of reactants to a high yield under conditions that reduce the occurrence of secondary reactions that could otherwise produce unwanted byproducts. The circulating fluidized bed

reactor section maintains nearly plug flow conditions that allow continued conversion of unreacted feed components through primary reactions while limiting the time for secondary reactions to continue and diminish the final yield of products. Selectivity and conversion may also be improved by sequential addition of oxygen into the CFB reaction section. The sequential addition of oxygen may occur by the direct injection of an oxygen-containing gas or by the delivery of re-oxidized catalyst particles that are fully recharged with the lattice oxygen necessary for the reaction.

REFERENCE COUNT: 13 THERE ARE 13 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L10 ANSWER 22 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 2000:158434 CAPLUS

DOCUMENT NUMBER: 132:168252

TITLE: Neural network model based on partial least square for

fluidized bed reactor

Ding, Li-hua; Luo, Bao-lin; Luo, Wei AUTHOR(S):

CORPORATE SOURCE: Petrochemical Institute, East China University of

Science and Technology, Shanghai, 200540, Peop. Rep.

China

Shiyou Huagong (2000), 29(2), 121-125 CODEN: SHHUE8; ISSN: 1000-8144 SOURCE:

PUBLISHER: Shiyou Huagong Bianjibu

DOCUMENT TYPE: Journal LANGUAGE: Chinese

Partial least square(PLS) is capable of projecting the information in high dimensional space down to low dimensional space and neural networks have universal approximation nonlinear property. The paper discusses the combination algorithm of neural network and PLS. A neural network model of the fluidized bed reactor based on partial least square proposed by using the exptl. data of the fluidized bed reactor for the synthesis of acrylonitrile from ammoxidn. of propylene. The simulation results show the proposed model is effective.

L10 ANSWER 23 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1999:811125 CAPLUS

DOCUMENT NUMBER: 132:36173

TITLE: Recovery of acrylonitrile

Ward, Gregory J.; Monical, Valerie S. INVENTOR(S):

Solutia Inc., USA PATENT ASSIGNEE(S): SOURCE: PCT Int. Appl., 12 pp.

CODEN: PIXXD2

DOCUMENT TYPE: Patent LANGUAGE: English

FAMILY ACC. NUM. COUNT: 2

PA	PENT	NO.			KIN	D	DATE		4	APPL	ICAT	ION	NO.		D.	ATE	
WO	9965	583			A1	-	1999	1223	1	wo 1	999-1	US13	 503		1	9990	615
	W:	ΑE,	AL,	AM,	AT,	AU,	AZ,	BA,	BB,	BG,	BR,	BY,	CA,	CH,	CN,	CU,	CZ,
		DE,	DK,	·EE,	ES,	FI,	GB,	GD,	GE,	GH,	GM,	HR,	HU,	ID,	IL,	IN,	IS,
		JP,	ΚE,	KG,	KP,	KR,	ΚZ,	LC,	LK,	LR,	LS,	LT,	LU,	LV,	MD,	MG,	MK,
		MN,	MW,	MX,	NO,	NZ,	PL,	PT,	RO,	RU,	SD,	SE,	SG,	SI,	SK,	SL,	TJ,
		TM,	TR,	TT,	UA,	UG,	UZ,	VN,	YU,	ZA,	zw						
	RW:	GH,	GM,	KE,	LS,	MW,	SD,	SL,	SZ,	ŪG,	ZW,	AT,	BE,	CH,	CY,	DE,	DK,
		ES,	FI,	FR,	GB,	GR,	IE,	IT,	LU,	MC,	NL,	PT,	SE,	BF,	ВJ,	CF,	CG,
		CI,	CM,	GA,	GN,	ĠW,	ML,	MR,	NE,	SN,	TD,	TG					
AU	9948	232			Α		2000	0105	2	AU 1	999-	4823	2		. 1	9990	615
BR	9911	267			Α		2001	0313	:	BR 1	999-	1126	7 ·		1	9990	615
TR	2000	0376	7		T2		2001	0321	•	rr 2	000-	2000	0376	7	1	9990	615

, EP	1093389	A1 ,	20010425	EP 1999-931802	•	19990615
EP	1093389	B1	20040324			
	R: DE, ES, IT	r, NL ·		•		,
JP	2002518353	Т.	20020625	JP 2000-554455		19990615
RU	2210566	C2	20030820	RU 2001-101465		19990615
ES	2214864	. T3	20040916	ES 1999-931802		19990615
RO	121093	B1	20061229	RO 2000-1238		19990615
BG.	. 105057	A	20011130	BG 2000-105057		20001215
BG	64862	B1	20060731			
MX	2000PA12649	· A	20011011	MX 2000-PA12649		20001218
PRIORIT	Y APPLN. INFO.:	•	•	US 1998-89352P	P	19980615
				WO 1999-US13503	W	19990615

AB A process for the recovery of acrylonitrile from an ammoxidn. reactor effluent stream containing acrylonitrile, water, and organic impurities includes passing an absorber bottoms stream through a single recovery/stripper column, generating an acrylonitrile-rich overhead stream, a lean water side stream, and a recovery/stripper bottoms stream containing organic impurities, wherein the acrylonitrile-rich overhead stream is passed into a condenser and into a decanter to sep. water from the acrylonitrile. The process can achieve the desired level of product recovery without requiring both a recovery distillation column and a stripper distillation column.

REFERENCE COUNT:

THERE ARE 4 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L10 ANSWER 24 OF 61 CAPLUS. COPYRIGHT 2007 ACS on STN

4

ACCESSION NUMBER:

1999:90417 CAPLUS

DOCUMENT NUMBER:

130:110732

TITLE:

Oxygen addition in an ammoxidation reaction to reduce

inert product formation in an acrylonitrile

reactor

INVENTOR(S):

Wagner, Matthew Lincoln

PATENT ASSIGNEE(S):

Praxair Technology, Inc., USA

SOURCE:

Eur. Pat. Appl., 5 pp.
CODEN: EPXXDW

DOCUMENT TYPE:

Patent

LANGUAGE:

English

DANTEN ACC NUM CON

1

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

	R: AT, BE IE, SI US 5883281 CN 1206708 CA 2243871 BR 9802595																
PAT	CENT :	NO.			KIN	D	DATE		7	APE	LICAT	NOI	NO.		D	ATE	
						_			-						_		
EP	8934	35			A2		1999	0127	H	ΞP	1998-	1138	28		1	9980	723
EP	•				A3		1999	1229									
	R:	AT,	BE,	CH,	DE,	DK,	ES,	FR,	GB,	GF	R, IT,	LI,	LU,	NL,	SE,	MC,	PT,
		ΙE,	SI,	LT,	LV,	FI,	RO			•							
US	5883	281			Α		1999	0316	ι	JS	1997-	8988	56		1	9970	725
CN	1206	708			Α		1999	0203		CN	1998-	1161	57		1	9980	722
CA	2243	871			A 1		1999	0125		CA	1998-	2243	871 [°]		1	9980	723
BR	9802	595			Α		2000	1205	E	3R	1998-	2595			1	9980	723
PRIORITY	APP	LN.	INFO	. :					Ţ	JS	1997-	8988	56		A 1	9970	725

AB A process for increasing the yield of an ammoxidn. product by passing a feed into a reactor, passing an oxygen-containing gas stream containing a portion of inerts into the reactor, passing a substantially pure oxygen stream into the reactor, and reducing the flow of the oxygen-containing gas stream while increasing the flow of the substantially pure oxygen stream, where the total rate of flow of oxygen from the oxygen-containing gas stream and the substantially pure oxygen stream is maintained in an effective amount to produce the ammoxidn. product such that the flow of inert materials passing into the reactor is reduced.

L10 ANSWER 25 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN DUPLICATE 1

ACCESSION NUMBER: 1999:511972 CAPLUS

DOCUMENT NUMBER: 131:242896

TITLE: Propane ammoxidation on an Al-Sb-V-W oxide catalyst. A

mechanistic study using the TAP-2 reactor system

AUTHOR(S): Hinz, Andreas; Andersson, Arne

CORPORATE SOURCE: Department of Chemical Engineering II, Chemical

Center, Lund University, Lund, S-221 00, Swed.

SOURCE: Chemical Engineering Science (1999), 54(20), 4407-4421 CODEN: CESCAC; ISSN: 0009-2509

PUBLISHER: Elsevier Science Ltd.

DOCUMENT TYPE: Journal LANGUAGE: English

The reaction mechanism of propane ammoxidn. was studied on an Al-Sb-V-W oxide catalyst using a TAP-2 reactor system. Analyses of the responses from both high-speed pulse transients with reactants and TPD expts. were .performed. Since the ammoxidn. process with three reactants proceeds from propane to acrylonitrile over propylene as an intermediate, the expts. comprised oxidation of propylene, oxidation of ammonia, ammoxidn. of propylene, oxidation of propane, and ammoxidn. of propane. The results show that propane is irreversibly adsorbed at the surface forming propylene, which desorbs. Propylene then readsorbs forming an intermediate allyl species, which reacts with lattice oxygen to give acrolein. Acrolein is unstable and some of it reacts further to produce either carbon oxides, or, acrylonitrile. Formation of the nitrile occurs by adsorbed acrolein reacting with an NHx species. The latter species is short-lived and reacts competitively to form N2, N2O and NO. Lattice oxygen plays an important role in the pathway to acrylonitrile. However, weakly adsorbed oxygen species are also present at the catalyst surface, and these species participate in degradation routes producing waste products. Consideration of the mechanistic scheme which is derived from the exptl. results shows the possibility to achieve improvement of the ammoxidn, process by using either a recirculating solids reactor, or a high propane/oxygen ratio in the feed.

REFERENCE COUNT: 39 THERE ARE 39 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L10 ANSWER 26 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1999:47696 CAPLUS

DOCUMENT NUMBER:

130:223615

TITLE:

Improving conversion and selectivity of catalytic

reactions in bubbling gas-solid fluidized bed reactors

by control of the nonlinear bubble dynamics

AUTHOR(S):

Kaart, Sander; Schouten, Jaap C.; van den Bleek, Cor

Μ.

CORPORATE SOURCE:

Department of Chemical Process Technology, Delft

University of Technology, Delft, 2628 BL, Neth.

SOURCE: Catalysis Today (1999), 48(1-4), 185-194

CODEN: CATTEA; ISSN: 0920-5861

PUBLISHER: Elsevier Science B.V.

DOCUMENT TYPE: Journal LANGUAGE: English

AB A model is presented that is a dynamic extension of the classic two-phase reactor models used to predict conversion and selectivity of fluidized reactors. The most important part of the model is a dynamic discrete bubble model that can correctly predict bubble sizes and also exhibits chaotic dynamics. The model is used to predict the effect of changed bubble dynamics on the catalytic ammoxidn. of propylene to acrylonitrile (Sohio process). Both conversion and selectivity are appreciably enhanced.

REFERENCE COUNT:

THERE ARE 21 CITED REFERENCES AVAILABLE FOR THIS RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L10 ANSWER 27 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

1999:76792 CAPLUS ACCESSION NUMBER:

DOCUMENT NUMBER:

130:223622

TITLE:

SOURCE:

Macroscopic regressive model of a fluidized-bed

reactor for synthesizing acrylonitrile by

ammoxidation of propylene

AUTHOR (S):

CORPORATE SOURCE:

Luo, Baolin; Yu, Jiangping; Fan, Zheng; Liu, Jinzhong

Inst. Chem. Metall., Chinese Academy of Sciences,

Beijing, 100080, Peop. Rep. China Huagong Yejin (1999), 20(1), 44-50

CODEN: HUYEEF; ISSN: 1001-2052

PUBLISHER:

Kexue Chubanshe

DOCUMENT TYPE:

LANGUAGE:

Journal Chinese

The kinetic behavior of the ammoxidn. of propylene was exptl. investigated and a math. model of reaction conversion rate and yield with power function is proposed. Using operating data from an industrial reactor and considering the effect of gas-solid flow in the reactor, the Marquardt method for nonlinear regression was used for establishing a macroscopic math. model of a fluidized-bed reactor for the preparation of acrylonitrile. The model fits exptl. data quite well with relative error <10%.

L10 ANSWER 28 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

1998:774318 CAPLUS

DOCUMENT NUMBER:

129:344717

TITLE:

Recovery of hydrogen cyanide from

acrylonitrile- and/or methacrylonitrile-

manufacture ammoxidation process effluent streams Sockell, Edward J.; Sarna, Joseph C.; Kerr, Ali;

Godbole, Sanjay P.

USA

PATENT ASSIGNEE(S): SOURCE:

U.S., 4 pp.

CODEN: USXXAM

DOCUMENT TYPE:

INVENTOR(S):

Patent

LANGUAGE:

English ·

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

P.	AT	ENT :	NO.			KIN	D	DATE		AP	PL]	ICAT	ION 1	NO.		D	ATE		
U.	 s	5840	955			 А		1998	1124	US	19	997-	 9777	 62		1:	9971	125	
E	Р	9195	43			A2		1999	0602	EP	19	998-	3071	18		1	9980	904	
· E	Р	9195	43			А3		2002	0807										
E	Р	9195	43			В1		2005	1123										
		R:	AT,	BE,	CH,	DE,	DK,	ES,	FR,	GB, G	R,	IT,	LI,	LU,	NL,	SE,	MC,	PT,	
			IE,	SI,	LT,	LV,								•	•	•	•	•	
A'	Т	3107	20			T		2005	1215	AT	19	998-	3071	18		1:	9980	904	
E	S	2252	818			т3		2006	0516	ES	19	998-	3071	18		1:	9980	904	
I	N	1998	DE02	652		Α		2005	0826	IN	19	998-	DE26	52		1	9980	907	
В	R	9803	782			Α		1999	1214	BR	19	998-	3782			1	99809	914	
C	N	1225	921			Α		1999	0818	CN	19	998-	1195	33		19	99809	917	
C	N	1117	072			В		2003	0806										
T	W	4081	01			В		2000	1011	TW	19	998-	8711	5520		19	99809	917	
J	Р	1119	9559			Α		1999	0727	JP	19	998-	2655	24		19	9809	918	
PRIORI'	ΤY	APP	LN.	INFO	. :					US	19	997-	9777	62	Į	A 19	971:	125	

AB A process for the enhanced recovery of hydrogen cyanide obtained from the reactor effluent of an ammoxidn. reaction of propylene or isobutylene comprises passing the reactor effluent through a quench column, an absorber column, a first distillation column, a second distillation

column, a cooler, and a knock-out pot, where the improvement consists of contacting the vapor phase containing the hydrogen cyanide with an aqueous stream.

This method achieves a higher degree of recovery of hydrogen cyanide, which is very useful as an industrial intermediate, than do prior-art processes and thus improves ammoxidn. process economics.

REFERENCE COUNT:

THERE ARE 13 CITED REFERENCES AVAILABLE FOR THIS 13 RECORD. ALL CITATIONS AVAILABLE IN THE RE FORMAT

L10 ANSWER 29 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

1998:217447 CAPLUS

DOCUMENT NUMBER:

128:230822

TITLE:

Ammoxidation in fluidized-bed

reactors

INVENTOR(S):

Nakamura, Toshio; Murata, Hiroshi; Nishijima, Katsumasa; Yamaguchi, Masanori; Sawada, Yoshikazu

PATENT ASSIGNEE(S):

Nitto Kagaku Kogyo K. K., Japan

SOURCE:

Eur. Pat. Appl., 19 pp.

CODEN: EPXXDW

DOCUMENT TYPE:

Patent

LANGUAGE:

English

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PA!	rent no	٠.			KINI	D DATI	<u> </u>	AP	PLICAT	ION I	NO.			DATE	
EP	832877				A2	1998	30401	EP	1997-	-3074	 83			19970	924
EP	832877				A3	1999	90127								
EP	832877				B1	2001	11121								
	R: A	Τ,	BE,	CH,	DE,	DK, ES,	FR,	GB, G	R, IT,	LI,	LU,	NL,	SE	, MC,	PT,
	I	E,	SI,	LT,	LV,	FI, RO									
JP	110433	23			Α	1999	90216	JP	1997-	-2102	20			19970	722
JP	101524	63			Α	1998	30609	JP	1997-	-2076	37			19970	801
JP	309116	8			B2	2000	00925								
ES	216695	3			тЗ	2002	20501	ES	1997-	3074	83			19970	924
NL	100712	0			A1	1998	30326	NL	1997-	-1007	120		·	19970	925
NL	100712	0			C2	1999	90223								
US	605747	1		٠	A	2000	0502	US	1997-	9369	11			19970	925
PRIORITY	Y APPLN	. I	NFO.	. :				JP	1996-	2534	91		A	199609	925
								JP	1997-	-2102	20		Α	19970	722
*								JP	1997-	-2076	37		A	19970	801

MeOH and hydrocarbons such as propylene and isobutylene are ammoxidized in AB a a fluidized-bed reactor to which an oxygen-containing gas is fed through feed openings provided at the bottom thereof, and a starting material to be ammoxidized is fed through feed openings provided above the feed openings for the oxygen-containing gas, the distance between the feed openings for the oxygen-containing gas and those for the starting material being from 30 to 250% of the height of a fluidized solid matter in a static state so as to form such a fluidized bed that the d. of the fluidized solid matter at the feed openings for the starting material to be ammoxidized is in the range of 50 to 300 kg/m3 and that the gas velocity is 1 m/s or lower. By this method, the efficiency of contact between catalyst particles and a starting material, and the result of the reaction (the yield of a desired product) are improved. HCN and acrylonitrile are manufactured from MeOH and propylene, resp.

L10 ANSWER 30 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

1998:230402 CAPLUS

DOCUMENT NUMBER:

128:257709

TITLE:

Review on fluidized bed reactor for propene

ammoxidation

AUTHOR(S):

Hong, Hui

CORPORATE SOURCE: Technology Development Center, SINOPEC, Beijing,

100029, Peop. Rep. China

SOURCE: Shiyou Huagong (1998), 27(3), 221-225 CODEN: SHHUE8; ISSN: 1000-8144

Beijing Huagong Yanjiuyuan
Journal; General Review

DOCUMENT TYPE: LANGUAGE:

PUBLISHER:

AB A review with 13 refs. on fluidized-bed reactors for ammoxidn. of propene to acrylonitrile.

L10 ANSWER 31 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

Chinese

ACCESSION NUMBER: 1997:503567 CAPLUS

DOCUMENT NUMBER: 127:123277

TITLE: Method for preparing vanadium-based

ammoxidation catalysts for a fluidized-bed or

APPLICATION NO

moving-bed reactor

חשתב

INVENTOR(S): Blanchard, Gilbert; Burattin, Paolo; Cavani, Fabrizio;

Masetti, Stefano; Trifiro, Ferruccio

PATENT ASSIGNEE(S): Rhone-Poulenc Fiber and Resin Intermediates, Fr.

SOURCE: PCT Int. Appl., 20 pp.

CODEN: PIXXD2

KIND

DOCUMENT TYPE: Patent LANGUAGE: French

FAMILY ACC. NUM. COUNT: 1

PATENT INFORMATION:

	PA:	LENT.	NO.			KIN.		DATE		А	.PE	LICATI	ON NO	•		DATE		
	WO					A1				W	0	1996-F	R2022		_	19961	218	
								, SG,										
					CH,							3, GR,						SE
	FR	2742	678	•		A1		1997	0627	F	R	1995-1	5783			19951	222	
	FR	2742	678					1998	0220									
	TW	4158	55			В		2000	1221	T	W	1996-8	511552	27		19961	216	
	CA	2239	102			A1		1997	0703	. C.	Α	1996-2	239102	2		19961	218	
	CA	2239	102		•	С		2001	0619									
	ΕP	8762	10			A 1		1998	1111	E	Р	1996-9	42424	•		19961	218	
	EP	8762	10			В1		2001	0425									
		R:	BE,	DE,	FR,	GB,	IT	, NL										
		1205							0120	C	N	1996-1	99203			19961	218	
	CN	1084	221			В		2002	0508									
	JΡ	2000	5006	599		т		2000	0125	J	Р	1997-5	23355			19961	218	
		3320						2002	0903									
	US	6200	926			В1		2001	0313	U	S	1996-7	69446			19961	219	
PRIO	RIT	APP	LN.	INFO	. :					F	R	1995-1	5783		Α	19951	222	
										U	S	1996-1	5479P		Р	19960	412	
												1996-F				19961		
													•					

Alkane ammoxidn. catalysts including mixed oxides based on vanadium, antimony and optionally tin and/or titanium and/or iron and/or other metals on a carrier are prepared by impregnating a solid oxide carrier with a solution of resp. vanadium, antimony or optionally tin and/or titanium and/or iron and/or other metal compds. in at least one saturated alc., contacting the resulting impregnated solid carrier with an aqueous buffer solution having a pH of 6 to 8, separating and drying the solid, and calcining

the

solid in two stages, firstly at 300-350 °C, and then at 400-800 °C. Such catalysts are suitable for use in a fluidized or moving bed. Propane was ammoxidized to acrylonitrile using a VSb5Sn5Ox catalyst.

L10 ANSWER 32 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN ACCESSION NUMBER: 1998:15739 CAPLUS

DOCUMENT NUMBER:

128:89221

TITLE:

Acrylonitrile recovery process

INVENTOR(S):

Wachtendorf, Paul Trigg; Godbole, Sanjay Parushottam;

Rinker, Jeffrey Earle Standard Oil Co., USA

PATENT ASSIGNEE(S):

SOURCE:

U.S., 3 pp. CODEN: USXXAM

DOCUMENT TYPE:

Patent

LANGUAGE:

English

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

	PA:	CENT	NO.			KIЙI	DAT	'E	AP	PLICAT	ION I	NO.		D	ATE	
	US	5703	268			 А	199	71230	US	1996-	6291	- -		19	99604	108
	JΡ	1103	5543			Α	199	90209	JP	1997-	1828	28		19	99707	708
	EP	8919	67			A 1	199	90120	EP	1997-	3054	16		19	99707	118
	ΕP	8919	67			В1	200	60927				•				
		R:	AT,	BE,	CH,	DE,	DK, ES	, FR,	GB, G	R, IT,	LI,	LU,	NL,	SE,	MC,	PT,
			IE,	SI,	LT,	LV,	FI, RO)								
	BR	9704	100			Α	199	90202	BR	1997-	4100			19	99707	25
	CN	1207	386			Α	199	90210	CN	1997-	1173	71		19	99708	306
	CN	1121	382			В	200	30917								
	TW	3947	55			В	200	00621	TW	1997-	8611	1238		19	9708	106
	RU	2196	766			C2	200	30120	RU	1997-	1136	80		19	99708	106
	RO	1209	08			В1	200	60929	·RO	1997-	1489			19	99708	06
PRIO	RITY	APP	LŊ.	INFO	. :				US	1996-	6291	29	7	19	99604	80

AB In a process for the recovery of CH2: CHCN or CH2: CMeCN obtained from the reactor effluent of an ammoxidn. reaction of propylene or isobutylene comprising passing the reactor effluent through an absorber column and recovery column and stripper column, the improvement comprises increasing the recovery column top pressure by mech. means by 0.1-5 psi to improve the hydraulic capacity of the recovery and stripper columns.

L10 ANSWER 33 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

1997:342011 CAPLUS

DOCUMENT NUMBER:

126:317181

TITLE:

Acrylonitrile and methacrylonitrile preparation and recovery process

INVENTOR(S):

Gibson, James S.; Rinker, Jeffrey E.; Wachtendorf,

Paul T.; Godbole, Sanjay P.

PATENT ASSIGNEE(S):

Standard Oil Company, USA

SOURCE:

U.S., 4 pp.

. CODEN: USXXAM

DOCUMENT TYPE:

Patent

LANGUAGE:

English

FAMILY ACC. NUM. COUNT:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
		'		
US 5629444	A	19970513	US 1996-659480	19960606
IN 1997DE00020	Α .	20050701	IN 1997-DE20	19970103
BR 9700013	Α	19981110	BR 1997-13	19970106
ZA 9700104	Α	19970716	ZA 1997-104	19970107
EP 811609	A2	19971210	EP 1997-300387	19970121
EP 811609	A3	19990113	•	
EP 811609	B1	20010620		
R: DE, ES, GB	, IT, NL			
ES 2158448	Т3	20010901	ES 1997-300387	19970121
JP 10007639	Α	19980113	JP 1997-12993	19970127

BG 62927	B1	20001130	BG 1997-101172	19970127
RO 118202	B1	20030328	RO 1997-145	19970127
TW 438743	В	20010607	TW 1997-86100910	19970128
RU 2178410	C2	20020120	RU 1997-101165	19970128
CN 1167757	A	19971217	CN 1997-102511	19970129
CN 1090175	В	20020904		
PRIORITY APPLN. INFO.:			US 1996-659480	A 19960606

AB A process for the recovery of acrylonitrile or methacrylonitrile, obtained from the reactor effluent of an ammoxidn. reaction of propylene or isobutylene, comprises passing the reactor effluent through an absorber column, a first decanter, a recovery column, a second decanter, and a stripper column, where the process improvement comprises maintaining the inside temperature of the first and second decanters at 32-75°F. A process flow diagram is presented.

L10 ANSWER 34 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

1996:607475 CAPLUS

DOCUMENT NUMBER:

125:222731

TITLE:

SOURCE:

Process for producing unsaturated nitriles

INVENTOR(S): Someya, Ken; Midorikawa, Hideo

PATENT ASSIGNEE(S):

Aşahi Kasei Kogyo Kabushiki Kaisha, Japan

PCT Int. Appl., 24 pp.

CODEN: PIXXD2

DOCUMENT TYPE:

Patent Japanese

LANGUAGE:

r. 1

FAMILY ACC. NUM. COUNT: 1

PATENT INFORMATION:

PA	rent n	10.			KINI	D I	DATE		P	APE	PLICAT	ION 1	10.			DATE		
WO	96237			WD.	A1		19960	808	W	10	1996-	JP14	3			19960	126	
•	W: RW:	•	•	•	,	SG, DK,		FR,	GB,	GF	R, IE,	IT,	LU,	MC,	NI	, PT,	SE	
IN	18488	31			A1	2	20001	L007	Ι	N	1996-0	CA10	5			19960	122	
EP	80762	22			A1	. 1	19971	L119	E	ΈP	1996-9	90112	23			19960	126	
EP	80762	22			В1	2	20020	731										
	R:	DE,	ES,	IT,	NL													
CN	11724	172			Α	· 1	19980	204	С	N	1996-3	1917	80			19960	126	
CN	10701	.72			В	2	20010	829		٠								
JP	32704	179			B2	2	20020	1402	J	Р	1996-5	52340	03			19960	126	
ES	21807	128			Т3	2	20030	216	E	S	1996-9	90112	23			19960	126	
US	60138	325			Α	2	20000	111	U	rs	1997-8	37589	98	•		19970	930	
PRIORITY	Y APPI	JN.	INFO	. :					J	Р	1995-3	3286	5	I	Ą	19950	131	
									W	10	1996-	JP148	3	V	7	19960	126	

AB A process for producing unsatd. nitriles such as acrylonitrile or methacrylonitrile by the ammoxidn. of organic compds. such as propylene, isobutene or tert-butanol, comprises conducting ammoxidn. in a reactor by controlling the ratio of the organic acids to the unreacted ammonia in the gas formed in the reaction to be in the range of 0.8-3.0, and leading the formed gas to a quenching tower, where the unreacted ammonia is reacted with the organic acids formed in the reactor to thereby fix the ammonia in the form of ammonium salts of the acids.

L10 ANSWER 35 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

1996:325662 CAPLUS

DOCUMENT NUMBER:

125:11510

TITLE:

Development and modeling of a loop fluidized bed reactor with baffle for propylene ammoxidation

AUTHOR(S):

Chen, B. H.; Dai, Q. L.; Lu, D. W.

CORPORATE SOURCE:

Department of Chemical Engineering, Zhejiang University, HangZhou, 310027, Peop. Rep. China

SOURCE: Chemical Engineering Science (1996), 51(11), 2983-2988

CODEN: CESCAC; ISSN: 0009-2509

PUBLISHER: Elsevier DOCUMENT TYPE: Journal LANGUAGE: English

A loop, with baffle, fluidized bed reactor (LBR) is proposed in this work. The reactor is developed to match the redox reaction mechanism of catalytic propylene ammoxidn. to acrylonitrile. According to its developmental concept, it is able to be applied not only in acrylonitrile synthesis via propylene ammoxidn. but also in most of olefins selective ammoxidn. and oxidation reactions. In this paper, the relationship between mass transfer coefficient, catalyst recycle rate and the internal structure, operating conditions are investigated in a \$\Phi300 mm cold model fluidized bed. The math. model is built up for the reactor. The computational results for propylene ammoxidn. based on this model show reasonable good agreement with the Φ 219 mm pilot plant data. prediction of larger scale plant based on this model has been done, and the $\Phi 2800$ mm pilot plant data. The prediction of larger scale plant based on this model has been done, and the $\Phi 2800$ mm pilot plant data are listed in this paper. The LBR is capable of increasing more than 2.5% selectivity to acrylonitrile when compared with the com. type reactor when it is employed in propylene ammoxidn.

L10 ANSWER 36 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1994:192557 CAPLUS

DOCUMENT NUMBER: 120:192557

TITLE: Process for the production of unsaturated nitriles

from a mixture of an alkene and an alkane

INVENTOR(S): Ramachandran, Ramakrishnan

PATENT ASSIGNEE(S): BOC Group, Inc., USA

PATENT ASSIGNEE(S): SOURCE:

U.S., 8 pp.

DOCUMENT TYPE:

CODEN: USXXAM Patent

LANGUAGE:

English

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
US 5268497	Α	19931207	US 1992-840363	19920224
ZA 9300281	Α	19931025	ZA 1993-281	19930115
JP 06009532	Α	19940118	JP 1993-33418	19930223
PRIORITY APPLN. INFO.:			US 1992-840363 A	19920224

AB The alkene in the feed mixture is converted to unsatd. nitrile by reaction with the oxygen and ammonia in the presence of a suitable catalyst in an ammoxidn. reactor; the nitrile product is recovered from the product stream; some of the byproduct carbon oxides and some of the inert gas introduced into the system with the reactants are removed from product stream and the remainder of the stream, now rich in unreacted alkene and alkane, and containing the rest of the byproduct gases and inert gases is introduced into a reactor which contains a catalyst that causes alkane contained in the gas stream to convert to the corresponding alkene. The effluent from the dehydrogenation reactor is recycled to the ammoxidn. reactor. A simulated feed containing 93 vol% C3H6 and 7% C3H8 was converted to acrylonitrile with conversion and selectivity 96 and 78, resp., and to C3H6 with conversion and selectivity 40 and 93%, resp.

L10 ANSWER 37 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1994:194507 CAPLUS

DOCUMENT NUMBER: 120:194507

TITLE: Production of unsaturated nitriles from alkenes and

alkanes

INVENTOR(S): Ramachandran, Ramakrishnan

PATENT ASSIGNEE(S): BOC Group, Inc., USA

SOURCE: U.S., 7 pp.
CODEN: USXXAM

DOCUMENT TYPE: Patent LANGUAGE: English

FAMILY ACC. NUM. COUNT: 1

PATENT INFORMATION:

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
	us 5264608 .	Α	19931123	US 1992-840484	19920224
	ZA 9300248	Α	19931025	ZA 1993-248	19930114
	JP 06009533	Α	19940118	JP 1993-33420	19930223
PRIO	RITY APPLN. INFO.:			US 1992-840484	A 19920224
AB	A feed stream conta	ining a	mixture of	an alkene and an all	kane is conver
	unsatd. nitrile by.	reactio	on with the c	xygen and ammonia in	n the presence
		2 4		1	=

rted to e of a suitable catalyst in a first ammoxidn. reactor; the nitrile product is recovered from the product stream; some of the byproduct carbon oxides and some of the inert gas introduced into the system with the reactants are removed from product stream and the remainder of this stream, now rich in unreacted alkene and alkane, and containing the rest of the byproduct gases and inert gases is introduced with addnl. oxygen-containing gas and ammonia into a second ammoxidn. reactor which contains a catalyst that catalyzes reaction between the alkane, oxygen and ammonia to produce addnl. unsatd. nitrile. effluent from the second ammoxidn. reactor is fully recycled to the first ammoxidn. reactor or to the nitrile recovery unit or it is split into 2 streams, one of which is recycled to the first ammoxidn. reactor and the other of which is recycled to the nitrile recovery unit. A feed stream containing C3H6 7.5, O 17.5, N 66.1, C3H8 0.6, and NH3 8.3% was converted in a 1st vapor phase fluidized bed reactor packed with supported mixed Fe-Sb oxides and then in a 2nd reactor packed with supported mixed V-Sb oxides, giving acrylonitrile with selectivity 67 and C3H6 conversion 96 in the 1st reactor and 60 and C3H8 conversion 67% in the 2nd reactor, resp.

L10 ANSWER 38 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1991:229611 CAPLUS

DOCUMENT NUMBER: 114:229611

TITLE: Apparatus for preparing α, β -unsaturated

nitriles by ammoxidation

INVENTOR(S): Muroya, Hiroaki; Ishii, Kanji; Ohta, Masanobu; Tanaka,

Tetsuo

PATENT ASSIGNEE(S): Asahi Chemical Industry Co., Ltd., Japan

SOURCE: PCT Int. Appl., 31 pp.

CODEN: PIXXD2

DOCUMENT TYPE: Patent LANGUAGE: Japanese

FAMILY ACC. NUM. COUNT: 1

PATENT NO.	KIND DAT	E APPLICATION NO.	DATE
WO 9104961 W: CA, KR, SU,		10418 WO 1990-JP1279	19901004
, , ,		, FR, GB, IT, LU, NL, SE	
JP 03120247	A 199	10522 JP 1989-257899	19891004
JP 03123767	A 199	10527 JP 1989-258908	19891005
CA 2042584	A1 · 199	10405 CA 1990-2042584	19901004
CA 2042584	C 199	31109	

EP 446379			1990-914763		19901004
EP 446379	B1 19	9940406			
R: DE, ES, FR,	GB, IT, 1	۷L			
ES 2051025	T3 19	9940601 ES	1990-914763		19901004
SU 1829957	A3 19	9930723 SU	1991-4895746		19910603
PRIORITY APPLN. INFO.:		JP	1989-257899	Α	19891004
		JP	1989-258908	Α	19891005
		WO	1990-JP1279	W	19901004

AB A reactor for the preparation of acrylonitrile or methacrylonitrile by gas-phase ammoxidn. of propene, isobutylene, or Me3COH contains in its lower part multiple inlets for the starting gas and multiple inlets for O-containing gas arranged to face the inlets for the starting gas at a distance of 25-250 mm, the inlets being located 90-250 mm from each other with a d. of 16-120 inlets/m2 of the cross-section of the reactor.

L10 ANSWER 39 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

1991:409358 CAPLUS ACCESSION NUMBER:

DOCUMENT NUMBER: 115:9358

TITLE: Progress in acrylonitrile processes and its

development policy

Hong, Zhangchuan AUTHOR(S):

CORPORATE SOURCE: Anqing Pet. Cent. Co., Peop. Rep. China SOURCE: Xiandai Huagong (1990), 10(4), 27-31

CODEN: HTKUDJ; ISSN: 0253-4320

DOCUMENT TYPE: Journal; General Review

Chinese LANGUAGE:

A review with 6 refs. with emphasis on development of high-performance catalysts for ammoxidn. of propylene, modification of ammoxidn. reactor, and purification of acrylonitrile and its relative energy-saving measures.

L10 ANSWER 40 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

1990:99469 CAPLUS ACCESSION NUMBER:

DOCUMENT NUMBER: 112:99469

TITLE: Production of α,β -olefinically unsaturated

nitriles

INVENTOR(S): Ramachandran, Ramakrishnan; Malik, Virginia A.;

MacLean, Donald L.; Satchell, Donald P., Jr.

PATENT ASSIGNEE(S): BOC Group, Inc., USA

SOURCE: U.S., 14 pp.

CODEN: USXXAM

DOCUMENT TYPE: Patent LANGUAGE: English

FAMILY ACC. NUM. COUNT: PATENT INFORMATION:

	PA:	PENT	NO.			KINI	D.	DATE			API	PLICATI	ON N	ю.	•	DA	re	
	US	4870	201			 А	_	1989	0926		us	1988-2	28158	. -		198	3812	 08
		5008				A		1991				1989-4		_			39092	
•	·EP	3729	72			A1		1990	0613		ΕP	1989-3	31278	17		198	3912	07
	ĒΡ	3729	72			B1		1994	0202									
		R:	ΑT,	BE,	DE,	ES,	FR	, GB,	ΙΤ,	NL,	, SI	2						
	ZA	8909	381			Α		1990	1031		ZA	1989-9	381			198	39120	07
	ΑT	1011	22			T ·		1994	0215		ΑT	1989-3	31278	17		198	39120	07
	ES	2062	042			Т3		1994	1216		ES	1989-3	31278	7		198	39120	07
	JP	0222	3545			Α		1990	0905		JP	1989-3	32041	.1		198	39120	80
	JP	2731	612			В2		1998	0325									
PRIC	ORIT	Y APP	LN.	INFO	.:						US	1988-2	28158	1	A2	198	88120	80
					,						US	1989-4	11043	15	A	198	39092	21
•									•		ΕP	1989-3	31278	17	Α	198	39120	07
AB	Hid	rh-ef	fici	encv	and	hial	า-ร	electi	ivity	v ti	$it.1\epsilon$	proce	ess c	:ompri	ses	(A)	fort	ni no

an alkene from a gaseous alkane in a catalytic dehydrogenator; (B) introducing a stream of the resulting alkene, O or O-enriched gas, and NH3 to an ammoxidn. reactor, and reacting in the vapor phase to produce a gaseous effluent containing the nitrile; (C) quenching in a liquid to form a nitrile-containing liquid phase and a gaseous phase; (D) recovering the nitrile; (E) introducing the gaseous phase in C to a pressure swing adsorption to form a gaseous stream comprising unreacted alkane and alkene, a minor amount of O and N; (F) removing the remaining O in the stream by passing through a catalytic selective oxidation unit; and (G) recycling the effluent to the dehydrogenator. The improvement comprises ≥2 parts of series-connected adsorptive beds in the pressure swing adsorption unit, wherein the 1st prior preferentially adsorbs alkane and alkene to other gases, therefore forming a gaseous stream containing them and a vent stream containing O, H, and N, which is introduced to the 2nd pair, thereby forming a stream of O and N, and H-enriched stream.

L10 ANSWER 41 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1988:424495 CAPLUS

DOCUMENT NUMBER:

109:24495

TITLE:

Structure of active phases of cerium-containing

multicomponent oxide and its catalytic behavior for

ammoxidation of propylene

AUTHOR(S):

Zheng, Yuzhen; Yang, Tianrong; Yu, Zuolong; Zhao,

Jinglin; Cai, Hequan; Zhao, Qingyue

CORPORATE SOURCE:

Changchun Inst. Appl. Chem., Acad. Sin., Changchun,

Peop. Rep. China

SOURCE:

Yingyong Huaxue (1988), 5(2), 13-17

CODEN: YIHUED; ISSN: 1000-0518

DOCUMENT TYPE:

Journal

LANGUAGE:

Chinese The effect of Ce3+ on the catalytic behavior of multicomponent oxides consisting of PMo12Bi3Fe8-xCexK0.10y (I; x = 0-8) for ammoxidn.

of propylene was studied in a fluidized-bed reactor. The structure of the catalyst was characterized by X-ray diffraction, IR, SEM, and thermogravimetry. The highest yield of acrylonitrile was obtained for I (x = 2-3) with Fe2(MoO4)3, Ce2(MoO4)3, and $\alpha\textsc{-Bi2O3.3MoO3}$ also being present in the catalyst. The dissoln. and coagulation of the 3 phases in the solid solution and the formation of pseudohomogeneous phase made the active component uniformly distributed at the surface and boundaries of the phases. The activity of the catalysts was caused by synergistic effect of the individual active components. inhibited the sublimation of MoO3 and stabilized the structure of the active phases.

L10 ANSWER 42 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1986:609554 CAPLUS

DOCUMENT NUMBER:

105:209554

TITLE: INVENTOR(S): Unsaturated nitriles from alkanes Khoobiar, Sargis; Shapiro, Arnold J.

PATENT ASSIGNEE(S):

Halcon SD Group, Inc., USA

Eur. Pat. Appl., 18 pp. SOURCE:

CODEN: EPXXDW

DOCUMENT TYPE:

Patent English

LANGUAGE:

FAMILY ACC. NUM. COUNT: 1

PATENT INFORMATION:

PATENT NO.	· KIND	DATE	APPLICATION NO.	DATE

EP. 193310 19860903 EP 1986-300992 A1 19860213

R: BE, DE, FR, GB, IT, NL

US 4609502 19860902 US 1985-701725 19850214 JP 61189256 Α 19860822 JP 1985-225950 19880628 US 1986-830423 US 4754049 Α 19860218 PRIORITY APPLN. INFO.: US 1985-701725 A 19850214

CASREACT 105:209554; MARPAT 105:209554 OTHER SOURCE(S): Nitriles are prepared economically from the corresponding alkanes by (A) dehydrogenating the alkanes to olefins in the presence of steam and Group VIII metal catalysts to form an effluent stream comprising olefins, H, H2O, carbon oxides, light hydrocarbons, and unreacted alkanes, (B) passing the mixture of the effluent stream, O, and NH3 over an ammoxidn. catalyst to produce nitrile, (c) absorbing the nitrile to form an aqueous stream, (d) selectively oxidizing H from nitrile-depleted effluent over a catalyst, (e) separating carbon oxides and light hydrocarbons from the oxidized effluent, and (f) recycling the major part of the effluent containing alkane and olefin to the dehydrogenation reactor. Thus, 743 mol/h mixture of 14.9:7.1:0.7:9.2:6.9:0.8:36.4:23.9 (%) H/O/CH4/C2H6/CH2:CHCH3/H2O/carbon oxides/C3H8 was heated at 60° in a selective oxidation reactor, separated into a purge stream and a recycled stream containing 95% C3 compds., which was combined with 75.3 mol/h H2O(g) to form 798.4 mol/h mixture containing 6.3% CH2: CHCH3, 34.6% C3H8, and no O, and fed to a dehydrogenation reactor at 600° and 0.7 bar over Pt and Ti on Zn aluminate to form a stream containing CH2: CHCH3 (35.7% yield based on C3H8). This stream was cooled and mixed with 214.8 mol/h O, and 100.2 mol/h NH3 in ammoxidn. reactor at 405° over a catalyst to form H2C:CHCN (65.7%

yield based on CH2: CHCH3) which was absorbed and separated and the rest of the

L10 ANSWER 43 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1986:130295 CAPLUS

DOCUMENT NUMBER: 104:130295

TITLE: Adaptative control of a fluidized bed reactor AUTHOR(S): Koutchoukali, M. S.; Laguerie, C.; Najim, K.

CORPORATE SOURCE: Inst. Gen. Chim., Toulouse, 31078, Fr.

stream was recycled to the selective oxidation reactor.

SOURCE: IFAC Proceedings Series (1985), (4, Bridge Control

Sci. Technol.), 1863-6

CODEN: IPSEET; ISSN: 0741-1146

DOCUMENT TYPE: Journal LANGUAGE: English

AB The production of acrylonitrile [107-13-1] in a steel fluidized-bed reactor was controlled by application of self-tuning proportional, integral, and derivative controller. A math. model was proposed based on material and energy balances which gave a set of coupled nonlinear partial differential equations.

L10 ANSWER 44 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1986:7686 CAPLUS

DOCUMENT NUMBER: 104:7686

TITLE: Application of Kunii's bubble bed model to an

industrial fluid bed reactor

AUTHOR(S): Chowdhari, K. K.; Ponnani, K. N.

CORPORATE SOURCE: Res. Cent., Indian Petrochem. Corp. Ltd., Baroda, 391

346, India

SOURCE: Adv. Catal., [Proc. - Natl. Symp. Catal.], 7th (1985),

693-706. Editor(s): Prasada Rao, T. S. R. Wiley: New

York.

CODEN: 54LUA4

DOCUMENT TYPE: Conference LANGUAGE: English

AB C3H6 ammoxidn. to acrylonitrile in an industrial

fluidized-bed reactor was analyzed on the basis of the Kunii

bubble-bed model with modified estimation of the bubble diameter $% \left(1\right) =\left(1\right) +\left(1\right) +\left$

variation with the bed height, the conversion dependence on the bubble diameter, and the fluidization-velocity dependence on the bubble diameter are presented graphically.

L10 ANSWER 45 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1986:497977 CAPLUS

DOCUMENT NUMBER: 105:97977

TITLE: Mass catalyst for the acrylonitrile process

AUTHOR(S): Aranda, Ericka Diaz

CORPORATE SOURCE: Mex.

SOURCE: Revista del Instituto Mexicano del Petroleo (1985),

17(2), 52-63

CODEN: RVMPAX; ISSN: 0538-1428

DOCUMENT TYPE: Journal LANGUAGE: Spanish

AB A heterogeneous catalyst containing Sb204, Sn02, CuSb206 and Fe2Sb207 (after thermal activation) enhanced propylene [115-07-1] conversion and

minimized selectivity losses in acrylonitrile [107-13-1] production

by ammoxidn. in a fixed-bed reactor. The preparation of

the catalyst is described.

L10 ANSWER 46 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1984:513083 CAPLUS

DOCUMENT NUMBER: 101:113083

TITLE: A discrimination between some fluidized bed reactor

models for ammoxidation of propylene to

acrylonitrile

AUTHOR(S): Stergiou, L.; Laguerie, C.; Gilot, B.

CORPORATE SOURCE: Inst. Genie Chim., Chemin Loge, Toulouse, 31078, Fr.

SOURCE: Chemical Engineering Science (1984), 39(4), 713-30

CODEN: CESCAC; ISSN: 0009-2509

DOCUMENT TYPE: Journal LANGUAGE: English

AB The predictions of 4 fluidized bed reactor models were compared with exptl. results obtained for the catalytic ammoxidn. of propylene. None of the models were acceptable for the prediction of conversion rates over the whole range tested. The bubble assemblage model of K. Kato and C. Y. Wen (1969) gave the best overall predictions when modified to include the wakes of the bubbles with their clouds or the bubble formation diameter is reduced.

L10 ANSWER 47 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1984:493532 CAPLUS

DOCUMENT NUMBER: 101:93532

TITLE: An experimental evaluation of fluidized-reactor models

AUTHOR(S): Stergiou, L.; Laguerie, C.

CORPORATE SOURCE: Inst. Genie Chim., Toulouse, 31078, Fr.

SOURCE: Proc. Int. Conf. Fluid., 4th (1984), Meeting Date

1983, 557-64. Editor(s): Kunii, Daizo; Cole, Sanford

S. Eng. Found.: New York, N. Y.

CODEN: 52CZAS

DOCUMENT TYPE: Conference
LANGUAGE: English

AB Four fluidized bed reactor models are compared for the catalytic ammoxidn. of propylene to acrylonitrile in a 165-mm-diameter reactor. The bubble assemblage model of K. Kato and C. Y. Wen (1969) provides the best overall predictions of conversion if it is suitably modified to include

the wake with the bubble clouds.

L10 ANSWER 48 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN DUPLICATE 2

ACCESSION NUMBER: 1984:50850 CAPLUS

DOCUMENT NUMBER: 100:50850

TITLE:

Catalytic ammoxidation of propene in a

differential reactor

AUTHOR(S): ·

Stergiou, L.; Gilot, B.; Laguerie, C.

CORPORATE SOURCE:

Inst. Genie Chim., Toulouse, 31078, Fr.

SOURCE:

Chemical Engineering Journal (Amsterdam, Netherlands)

(1983), 26(3), 201-15

CODEN: CMEJAJ; ISSN: 0300-9467

DOCUMENT TYPE:

Journal French

LANGUAGE:

The ammoxidn. kinetics of MeCH: CH2 conversion to CH2: CHCN over a Sn/Sb oxide catalyst is determined in a differential reactor at 490°. Factorial design of expts. leads to reliable rate equations over the range of partial pressures encountered in a fluidized bed reaction. The catalyst selectivity at this temperature is ≥82%. The addition of steam reduces the catalyst activity but increases its selectivity for CH2: CHCN formation.

L10 ANSWER 49 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

1982:149895 CAPLUS

DOCUMENT NUMBER:

96:149895

TITLE:

Catalyst preparation technique

INVENTOR(S):

Miller, Arthur F.; Callahan, James L.; Shaw, Wilfrid

PATENT ASSIGNEE(S):

Standard Oil Co., USA

SOURCE:

U.S., 5 pp. CODEN: USXXAM

DOCUMENT TYPE:

Patent

LANGUAGE:

English

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.		DATE
					
US 4315838	Α	19820216	US 1978-912651		19780605
PRIORITY APPLN. INFO.:			US 1978-912651	A	19780605

A method for forming particle or bead catalysts for fixed-bed reactors, especially for ammoxidn. and oxidation, with higher yields and selectivities than

catalysts formed by conventional techniques consists of (1) forming a precatalyst containing all the catalytic metals and ≥1 thermally decomposable material, (2) optionally preheating to remove ≤90% of the decomposable material to form an aqueous slurry, (3) dropping slurry drops on a particle bed to from spherical agglomerates, and (4) calcining in O2 to form the catalyst. Thus, an ammoxidn. catalyst 82.5% Co4.5Ni2.5Fe3K0.07BiP0.5Mo12O50.3-17.5% SiO2 was formed by adding (NH4)6Mo7024.4H2O 4016 g to 8907 g H2O with stirring, adding H3PO4 109 g and Aerosil SiO2 soluble 555 g and stirring to a slurry, adding Co(NO3)3.6H2O 2482.5 g and Ni(NO3)3.6H2O 1378 g in 6325 g H2O, adding Fe(NO3)3.9H2O 2297 g in 422 g H2O, adding Bi(NO3)3.5H2O 919.5 g in 717 g H2O and 91.2 g HNO3, adding KNO3 171 g in 40 cm3 H2O, adding Aerosil 555 g with stirring for 30-45 min, spray drying and heating to remove 70-75% of the nitrates, adding 105 g H2O to 200 g of the denitrated powder and stirring to form a slurry, dropping the slurry onto a powder bed of the same composition, and heat treating to drive off the remaining nitrate.

L10 ANSWER 50 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

1983:161300 CAPLUS

DOCUMENT NUMBER:

98:161300

TITLE: INVENTOR(S): Apparatus for carrying out highly exothermic reactions Wittkopf, Manfred; Pohl, Dietrich; Knaack, Karl Ernst;

Kilian, Richard; Hebisch, Heinz; Mey, Frank;

Marschner, Rolf; Vettorazzi, Karl Heinz; Dobberstein,

Lutz; Et, Al.

PATENT ASSIGNEE(S):

Ger. Dem. Rep.

SOURCE:

Ger. (East), 14 pp. CODEN: GEXXA8

DOCUMENT TYPE:

Patent

LANGUAGE:

German

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
DD 157139	A 3	19821020	DD 1977-199138	19770526
PRIORITY APPLN. INFO.:			DD 1977-199138	19770526

AΒ The title reactor, giving better material exchange and control of reaction heat and especially useful in the ammoxidn. of propylene [115-07-1], contains phase-exchange tubes made of mesh or expanded metal which break up gas bubbles in fluidized beds. Thus, passing 1:1:9.5 C3H6-NH3-air through a catalytic reactor (length 1.5 m, diameter 80 mm) equipped with crosswise phase-exchange tubes 80 mm long and containing K0.07Ni2.5Co4.5Fe3BiMo12P0.50x catalyst (particle size 73% $40-90~\mu$) with contact time 10 s gave C3H6 conversion 96.5% and acrylonitrile [107-13-1] selectivity and yield 73.1 and 70.6%, resp., compared with 94.1, 68.8, and 64.8, resp., without the phase-exchange tubes.

L10 ANSWER 51 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

1982:562317 CAPLUS

DOCUMENT NUMBER:

97:162317

TITLE:

Experimental study on ammoxidation of propene to acrylonitrile in a laboratory-scale fluidized

bed reactor

AUTHOR(S):

Barbouteau, G.; Laguerie, C.; Cassimatis, D.;

Chavarie, C.

CORPORATE SOURCE:

Inst. Genie Chim., Toulouse, 31078, Fr.

SOURCE:

Bulletin de la Societe Chimique de France (1982),

(5-6, Pt. 1), I-202/I-210

CODEN: BSCFAS; ISSN: 0037-8968

DOCUMENT TYPE:

Journal

LANGUAGE:

French

Optimum conditions for ammoxidn. of propene to acrylonitrile in presence of Sn-Sb oxide catalyst were determined for a laboratory scale

fluidized bed

reactor. The maximum yield, 63%, was comparable to that obtained in a fixed bed reactor.

CAPLUS COPYRIGHT 2007 ACS on STN L10 ANSWER 52 OF 61

ACCESSION NUMBER:

CORPORATE SOURCE:

1981:3737 CAPLUS

DOCUMENT NUMBER:

TITLE:

Experimental comparison of the catalytic ammoxidation

of propene to acrylonitrile on a fixed bed

and on a fluidized bed

AUTHOR(S):

Barbouteau, G.; Laguerie, C.; Angelino, H. Inst. Genie Chim., Toulouse, 31078, Fr.

SOURCE:

Chemical Engineering Journal (Amsterdam, Netherlands)

(1980), 20(1), 43-57

CODEN: CMEJAJ; ISSN: 0300-9467

DOCUMENT TYPE:

Journal

LANGUAGE:

French

The ammoxidn. of propene over Sb-Sn-Fe-Cu catalyst in a 50 mm diameter fluidized bed reactor was comparable to the same process in a 25 mm diameter fixed bed reactor. The results were inferior in a 25 mm diameter fluidized bed reactor.

L10 ANSWER 53 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1979:459321 CAPLUS

DOCUMENT NUMBER: 91:59321

TITLE: Reactor for contacting gases and a particulate solid INVENTOR(S): Callahan, James L.; Hardman, Harley F.; Milberger,

Ernest C.

PATENT ASSIGNEE(S): Standard Oil Co., USA

SOURCE:

U.S., 8 pp. CODEN: USXXAM

DOCUMENT TYPE: Patent LANGUAGE: English

FAMILY ACC. NUM. COUNT: 1

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
				-
US 4152393	Α	19790501	US 1977-758607	19770112
US 4341717	Α	19820727	US 1978-967557	19781208
PRIORITY APPLN. INFO.:			US 1973-339082	Al 19730308
			US 1977-758607	A3 19770112

AB The reactor has a cylindrical shell and 3 concentric walls that form a central, cylindrical chamber and 3 annular chambers. The 1st and 3rd concentric walls are connected together around the lower end. The 2nd concentric wall extends downward from the cover into the space between the 1st and 3rd walls, but not to the bottom. Regeneration air is fed into the bottom zone of the central chamber and reactants are bed into the bottom zone of the chamber between the 1st and 3rd walls. The solids move upwardly in the central chamber and overflow into the adjacent annular chamber where they move downwardly and under the 2nd wall into the reaction chamber. The solids move upwardly in the reaction chamber and overflow into the outer chamber where they move downwardly to the reaction bottom and then horizontally into the bottom zone of the neutral chamber. The gases from the regeneration and reaction are discharged through cyclones and lines through the cover. The operation was exemplified on C3H6 ammoxidn. by NH3 and an oxidant consisting of K0.1Ni2.5Co4.5Fe3BiP0.5Mo12Ox 50 and SiO2 50% (particle size 74-177 μ). The C3H6 conversion was 89.0%, the selectivity to H2C:CHCN 64.4%, and the conversion/pass to H2C:CHCN 57.3%.

L10 ANSWER 54 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1980:59410 CAPLUS

DOCUMENT NUMBER: 92:59410

TITLE: Recovery and purification of olefinic nitriles

INVENTOR(S): Wu, Hsin C.

PATENT ASSIGNEE(S): Standard Oil Co., USA

SOURCE: Can., 17 pp. CODEN: CAXXA4

DOCUMENT TYPE: Patent LANGUAGE: English

FAMILY ACC. NUM. COUNT: 1

PATENT INFORMATION:

PATENT NO.	KIND ,	DATE	APPLICATION NO.	D.	ATE
				_	
CA 1063621	A1	19791002	CA 1975-239076	1	9751105
PRIORITY APPLN. INFO.:		•	CA 1975-239076 A	. 1	9751105

AB Recovery of acrylonitrile (I) [107-13-1] and methacrylonitrile (II) [126-98-7] produced by ammoxidn. of propylene [115-07-1] or isobutylene [115-11-7] is improved if at least part of the product distillation

column bottoms is recycled to form at least part of the quench liquid in the quenching step of a recovery system in which the ammoxidn.

reactor effluent is contacted with quench liquid to produce a gaseous effluent at 90-230°F, the gaseous effluent is absorbed in H2O, crude I or II is separated from impurities and most of the H2O, and the crude product is distilled to obtain a gaseous overhead stream of pure I or II and a column bottoms stream. This process improvement also eliminates the addnl. distillation step normally required for further recovery of I or II from the bottoms stream. A flow sheet diagram is included.

L10 ANSWER 55 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER:

1978:191767 CAPLUS

DOCUMENT NUMBER:

88:191767

TITLE:

Process for recovery and purification of olefinic

nitriles

INVENTOR(S):

Wu, Hsin Chih

PATENT ASSIGNEE(S):

Standard Oil Co., USA

SOURCE:

Brit., 6 pp. CODEN: BRXXAA

DOCUMENT TYPE:

Patent

LANGUAGE:

English

FAMILY ACC. NUM. COUNT:

PATENT INFORMATION:

	PATENT NO.	KIND	DATE .	APPLICATION NO.	DATE
		A-	19771116	GB 1975-47031	
PRIC	RITY APPLN. INFO.:			GB 1975-47031	
AB	An improved process	is des	cribed for	the recovery and pur	rification of
	acrylonitrile (I) f	rom the	ammoxidn.	of propylene by usin	ng the
				liquid Thus, efflue	
	ammoxidn. reactor w				
	to the top of a gas spray at 180°F. Hi	washer gh-boil	and was coning materia	ontacted with a recyc al collected at the k	oottom of
				re passed through a k	
				er-spray absorber. V	
	material was remove	ed from	the bottom	of the absorber and	passed into a
	recovery column fro	m which	volatile i	material was transfer	red to a HCN
	column and the bott	oms was	passed to	a stripper to remove	e acetonitrile.
				oray for the gas wash	
	ammoxidn. reactor e	ffluent	. I was re	ecovered from the	
	bottom of the HCN of	column a	nd was dis	tilled to remove wate	er and I loss was
	1.1% compared with				

L10 ANSWER 56 OF 61 COMPENDEX COPYRIGHT 2007 EEI on STN

ACCESSION NUMBER:

1977(9):1305 COMPENDEX

DOCUMENT NUMBER:

770967098

TITLE:

NEWEST ACRYLONITRILE PROCESS.

AUTHOR:

Pujado, P.R. (UOP Inc, Des Plaines, Ill); Vora, B.V.;

Krueding, A.P.

SOURCE:

Hydrocarbon Process v 56 n 5 May 1977 p 169-172 Hydrocarbon Process v 56 n 5 May 1977 p 169-172

CODEN: HYPRAX

PUBLICATION YEAR:

1977

LANGUAGE:

English

AN 1977(9):1305 COMPENDEX DN 770967098

AB A brief review of three methods of acrylonitrile synthesis is followed by a description of several modern commercial acrylonitrile processes based on propylene ammoxidation (oxidative amination). These processes are similar and can produce high purity product but each has its own characteristics of reaction techniques, catalyst, product recovery and purification. The ammoxidation catalyst and the reactor are the heart of the process. Some of the older ammoxidation processes used multi-tubular fixed-bed

reactors but all major modern acrylonitrile processes today use fluidized bed reactors. These reactors give much better temperature control and remove the limitations of propylene and ammonia concentration due to explosibility of the feed mixture in a fixed bed reactor. Details are given of the Montedison-UOP process which seems to be an attractive alternative to other existing technologies. The process is now operated in full-size commercial plants.

L10 ANSWER 57 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1975:532261 CAPLUS

DOCUMENT NUMBER: 83:132261

TITLE: Acrylonitrile and methacrylonitrile recovery

and purification system

INVENTOR(S): Wu, Hsin Chih

PATENT ASSIGNEE(S): Standard Oil Co., USA

SOURCE: U.S., 4 pp.
CODEN: USXXAM

DOCUMENT TYPE: Patent LANGUAGE: English

FAMILY ACC. NUM. COUNT: 1

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
US 3885928	Α	19750527	US 1973-371043	19730618
PRIORITY APPLN. INFO.:			US 1973-371043 A	19730618

The aqueous layer from the decanter used to sep. acrylonitrile
[107-13-1] or methacrylonitrile [126-98-7] from the sidestream from the
HCN distillation column which contained an acid stabilizer was recycled to the
quenching column to reduce the amount of acid necessary to neutralize the
excess NH3 coming from the ammoxidn. reactor. The
ammoxidn. reactor effluent was quenched in a column with
an aqueous medium to cool the hot gases, fed to an absorption column to
concentrate the nitrile-HCN mixture, fed to a distillation column where HCN was
removed, and AcOH was added to stabilize the system. A side or bottom
stream from the distillation column was fed to a decanter where the organic

was removed for further purification and the aqueous layer was recycled to the quenching column.

L10 ANSWER 58 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1976:422078 CAPLUS

DOCUMENT NUMBER: 85:22078

TITLE: Apparatus for acrylonitrile manufacture

INVENTOR(S): Tanaka, Tetsuo; Nogami, Akira

PATENT ASSIGNEE(S): Asahi Chemical Industry Co., Ltd., Japan

SOURCE: Jpn. Tokkyo Koho, 4 pp.

CODEN: JAXXAD

DOCUMENT TYPE: Patent

LANGUAGE: Facent
Japanese

FAMILY ACC. NUM. COUNT: 1

PATENT INFORMATION:

PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
JP 50015772	В	19750607	JP 1971-36284	19710528
PRIORITY APPLN. INFO.:			JP 1971-36284 A	19710528

AB Acrylonitrile (I) [107-13-1] was obtained in improved yield by ammoxidn. of propylene [115-07-1] in the presence of P-Mo-Bi/SiO2 catalyst by placing straight or U-shaped, vertical baffle pipes between cooling coil and air feeder in reactor; the baffle pipes occupied 5-40% of the reactor cross-sectional area. For example, in a 2.7 m-diameter reactor

filled with the catalyst to 3 m height (at rest) and containing U-shaped baffle pipes occupying 25% of the reactor cross-sectional area, the ammoxidn. of 500 m3/hr propylene with 5300 m3/hr air and 650 m3/hr NH3 at 400°/1 kg/cm2 gave products composed of I 63.5, MeCN 6.8, HCN 8.5, CO2 9.8, CO 7.4, and unreacted propylene 4.0, compared with 59, 7.0, 85, 10, 7.5, and 8.0, resp., for products obtained without the baffle pipes.

L10 ANSWER 59 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1975:72488 CAPLUS

DOCUMENT NUMBER: 82:72488

TITLE: Application of fluidized bed technology to

petrochemical reactions

AUTHOR(S): Holve, Wilbur A.; Sheely, H. Russell; Schaffert,

Frederich W., Jr.

Badger Co., Inc., Cambridge, MA, USA CORPORATE SOURCE:

SOURCE: Quaderni dell'Ingegnere Chimico Italiano (1974),

10(6), 112-14

CODEN: QICIAU; ISSN: 0370-288X

DOCUMENT TYPE: Journal LANGUAGE: Italian

The main characteristics of the fluidized bed reactor and of some of its industrial applications are briefly described. In particular, outlines of the following processes are reported: the oxidation of naphthalene to phthalic anhydride, the ammoxidn. of propylene to acrylonitrile, and the oxychlorination of ethylene to dichloroethane.

L10 ANSWER 60 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

ACCESSION NUMBER: 1970:54485 CAPLUS

DOCUMENT NUMBER: 72:54485

TITLE: Kinetics of the ammoxidation of propylene over a

bismuth-molybdate catalyst

AUTHOR(S): Shelstad, K. A.; Chong, T. C.

Fac. Eng. Sci., Univ. Western Ontario, London, ON, CORPORATE SOURCE:

Can.

SOURCE: Canadian Journal of Chemical Engineering (1969),

47(6), 597-602

CODEN: CJCEA7; ISSN: 0008-4034

DOCUMENT TYPE: Journal LANGUAGE: English

Integral conversion data for the ammoxidation of propylene were obtained using a flow reactor and 10.0 g of a bismuth-molybdate catalyst. Anal. by gas chromatog. for C-containing compds. in the product gases showed the presence of unreacted propylene, acrolein, acrylonitrile, CO2 and small amts. MeCN. The data at 390° were correlated on the basis of a simplified scheme of first-order reactions with acrolein as an intermediate. The results at higher temps. and with reduced amts. of O in the feed indicated that both the activity and selectivity of the catalyst were affected by the O content of the catalyst.

L10 ANSWER 61 OF 61 CAPLUS COPYRIGHT 2007 ACS on STN

Polish

1970:42712 CAPLUS ACCESSION NUMBER:

DOCUMENT NUMBER: 72:42712

Course of propene ammoxidation in a large TITLE:

laboratory reactor

AUTHOR(S): Wasilewski, Jerzy; Beres, Janusz; Spadlo, Marian

CORPORATE SOURCE: Inst. Ciezkiej Syn. Org., Blachownia Slaska, Pol. Przemysl Chemiczny (1969), 48(8-9), 523-7 SOURCE:

CODEN: PRCHAB; ISSN: 0033-2496

DOCUMENT TYPE: Journal

LANGUAGE:

AB Bi-Mo catalyst on α -Al2O3 carrier was used. The laboratory reactor, 25 mm

in diameter and one m operating length, had 8 sample outlets. Expts. were run at 490° and a mixture of 1:1:1.9:6.2 (molar ratio) C3H6-N H3-O2-H2O was fed at 1.97 moles C3H6/dm3/hr; 78.5% propene was converted to yield acrylonitrile 62.1, acetonitrile 8.7, HCN 7.0, and a mixture of CO and CO2 21.1%; selectivity of oxidation 79%; unit yield 65 g/dm/hr. From the exptl. results, math. relations, which could serve as a basis for a math. model for a tubular reactor as well as to verify the kinetics of formation of acrylonitrile, acetonitrile, HCN, and oxides of carbon, were formulated.

	Туре	L #	Hits	Search Text	DBs
1	BRS	L1	425	ammoxidation same reactor same acrylonitrile	US- PGPUB; USPAT; USOCR; FPRS; EPO; JPO; DERWEN T; IBM_TD B
2	BRS	L2	232	ammoxidation with reactor with acrylonitrile	US- PGPUB; USPAT; USOCR; FPRS; EPO; JPO; DERWEN T; IBM_TD B
3	BRS	L3	8	2 and spectrometer	US- PGPUB; USPAT; USOCR; FPRS; EPO; JPO; DERWEN T; IBM_TD B

	Туре	L #	Hits	Search Text	DBs
4	BRS	L4	8	2 and (spectrometer or spectrophotometer)	US- PGPUB; USPAT; USOCR; FPRS; EPO; DERWEN T; IBM_TD B
5	BRS	L5	4	("6284196").URPN.	USPAT
6	BRS	L6	1137	fourier near6 transform near6 infrared near6 (spectrometer or spectrophotometer)	USPAT
7	BRS	L7	2	reactor near8 effluent with fourier near6 transform near6 infrared near6 (spectrometer or spectrophotometer)	USPAT
8	BRS	L8	2	6 and ammoxidation	USPAT
9	BRS	L9	9 .	reactor with fourier near6 transform near6 infrared near6 (spectrometer or spectrophotometer)	USPAT
10	BRS	L10	3	reactor near8 effluent same fourier near6 transform near6 infrared near6 (spectrometer or spectrophotometer)	USPAT
11	BRS	L11	25	reactor same fourier near6 transform near6 infrared near6 (spectrometer or spectrophotometer)	USPAT